

UNIVERSITY OF CHEMISTRY AND TECHNOLOGY PRAGUE  
Faculty of Chemical Engineering  
Department of Chemical Engineering



# Advanced Pyrolysis Model Approach in FDS

*Author:*

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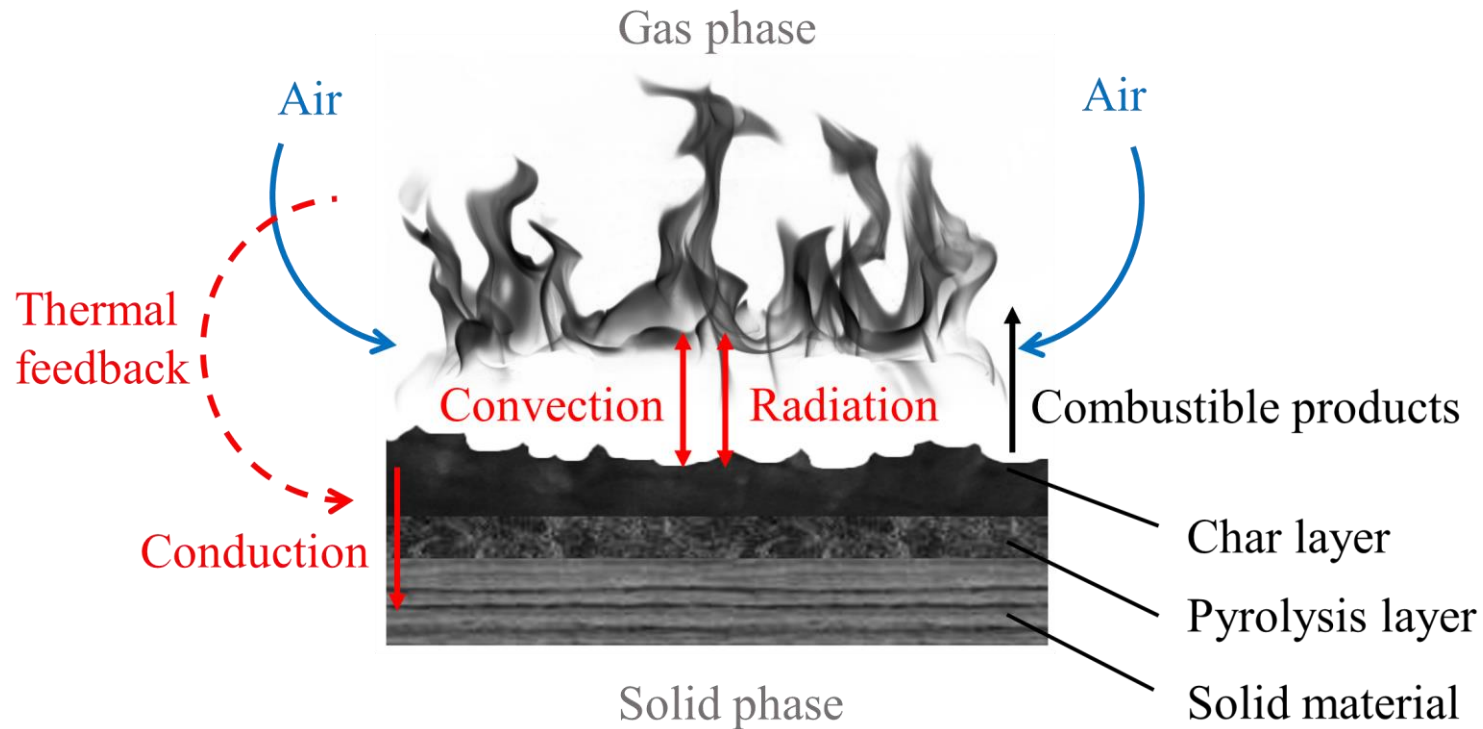
*Supervisor:*

*Assoc. Prof. Milan Jahoda*

*Supervisor-specialist:*

*Dr. Lucie Hasalová*

# Pyrolysis

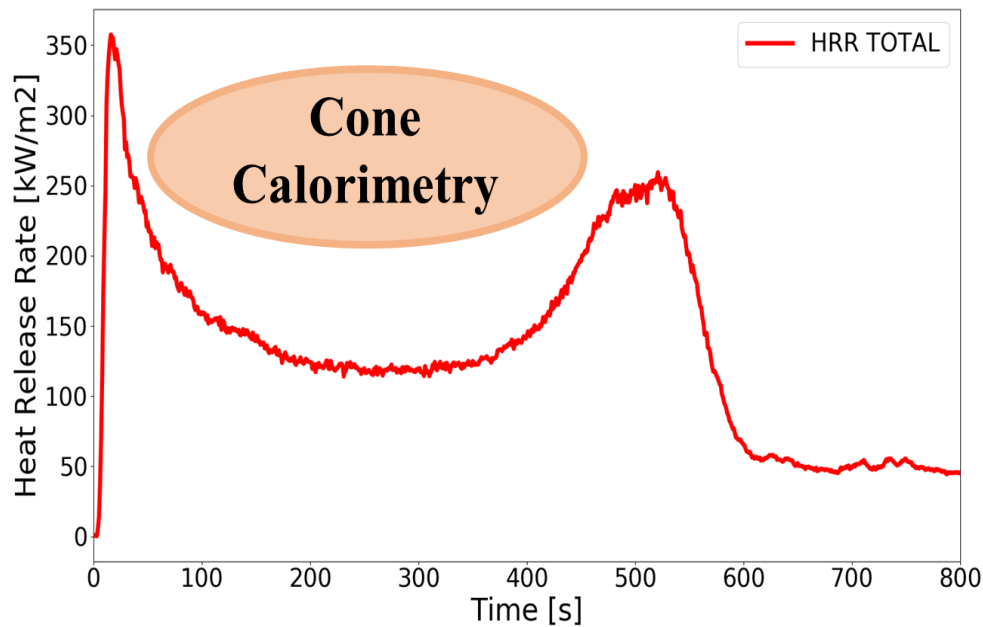


- Gaseous phase influence solid phase and vice versa
- How fast is gasification?  $\dot{m}$  (mass loss rate, MLR)
- FDS (Fire Dynamics Simulator)
- Different approaches (variously complex), **2** main

# Fire Consequence Modeling

- HRR (Heat release rate) -  $\dot{q}''$
- Heat of combustion -  $\Delta H_C$

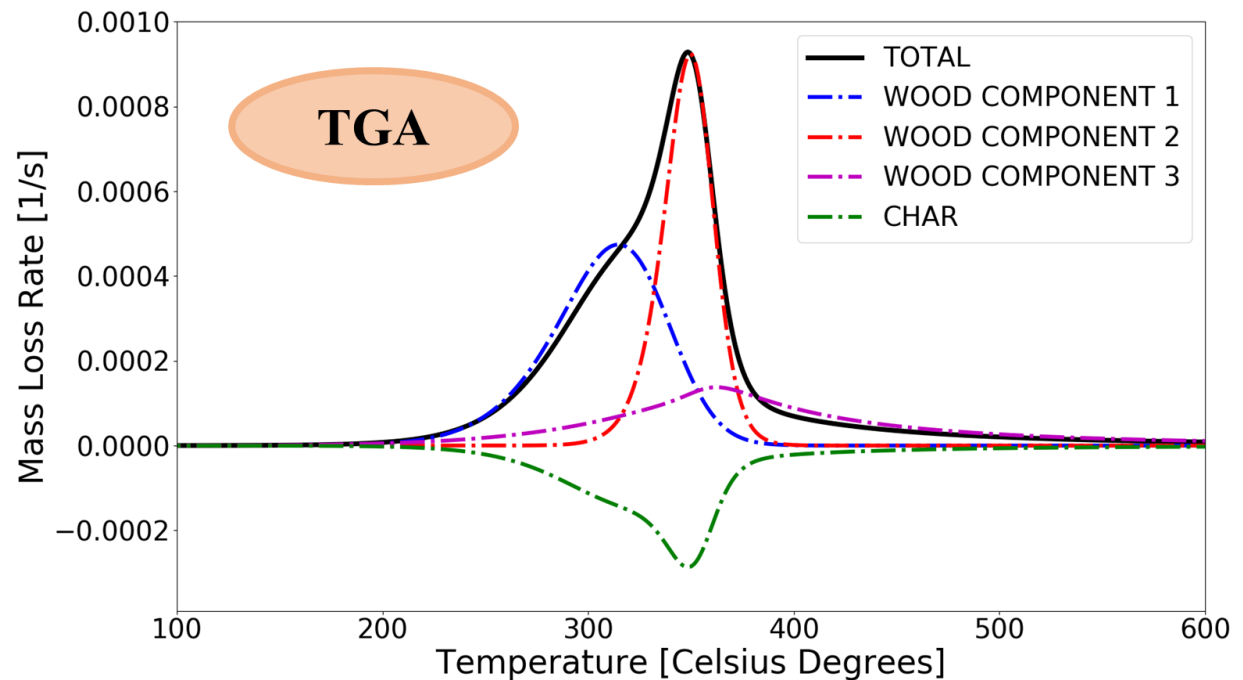
$$\dot{q}'' = \dot{m}\Delta H_C$$



ANAMET. Fire Testing Technology Ltd.  
<http://www.anamet.cz/vyrobce/fire-testing-technology-ltd> (cited 26.11.2019).

# Complex Pyrolysis Modeling

- Heat transfer, heat conduction, decomposition kinetics, combustion, smoke production and transport, etc.
  - > complicated – a lot of input parameters
- Both gas and solid phase solved at the same time



$v_1$  Wood component 1  $\longrightarrow$   $v_{CH,1}$  Char + Combustible gases  
 $v_2$  Wood component 2  $\longrightarrow$   $v_{CH,2}$  Char + Combustible gases  
 $v_3$  Wood component 3  $\longrightarrow$   $v_{CH,3}$  Char + Combustible gases

# Consequence vs. Complex Modeling

<i>Consequence modeling parameters</i>
Pyr. gas composition
Soot yield
Density
Heat conductivity
Specific heat
Emissivity
Heat release rate
Ignition temperature

11

vs.

30

<i>Complex modeling parameters</i>	<i>How to obtain</i>
Pyr. gas composition	El. analysis, lit.
Soot yield	Cone calorimetry
Density	Directly, lit.
Heat conductivity	Exp., literature
Specific heat	DSC, literature
Emissivity	Literature
Char density	Directly, lit.
Char heat cond.	Exp., literature
Char specific heat	DSC, literature
Char emissivity	Literature
Preexp. factor	TGA – opt.
Activation energy	TGA – opt.
Order of reaction	TGA – opt.
Heat of reaction	DSC
Heat of combustion	Cone calorimetry
Stoch. coeff. of char	TGA
Stoch. coeff. of decomposing comp.	TGA – opt.

- Is 11 enough? For which scenario?
- Validation!

# RCT (Room Corner Test)

- Test facility to determine Reaction to fire of facing materials (walls and ceilings)
- Burner location and fire load according to ISO 9705-1
- Room 2,4 x 3,6 x 2,4 m + hood 3 x 3 m + exhaust duct
- Walls covered by OSB board

INTERNATIONAL  
STANDARD

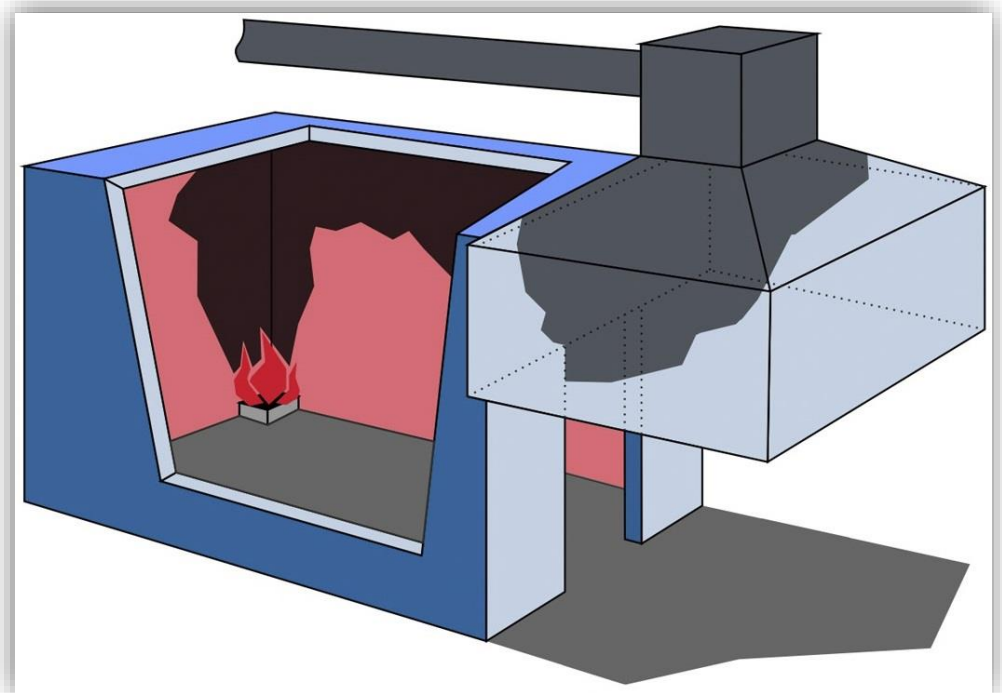
ISO  
9705-1

First edition  
2016-02-15

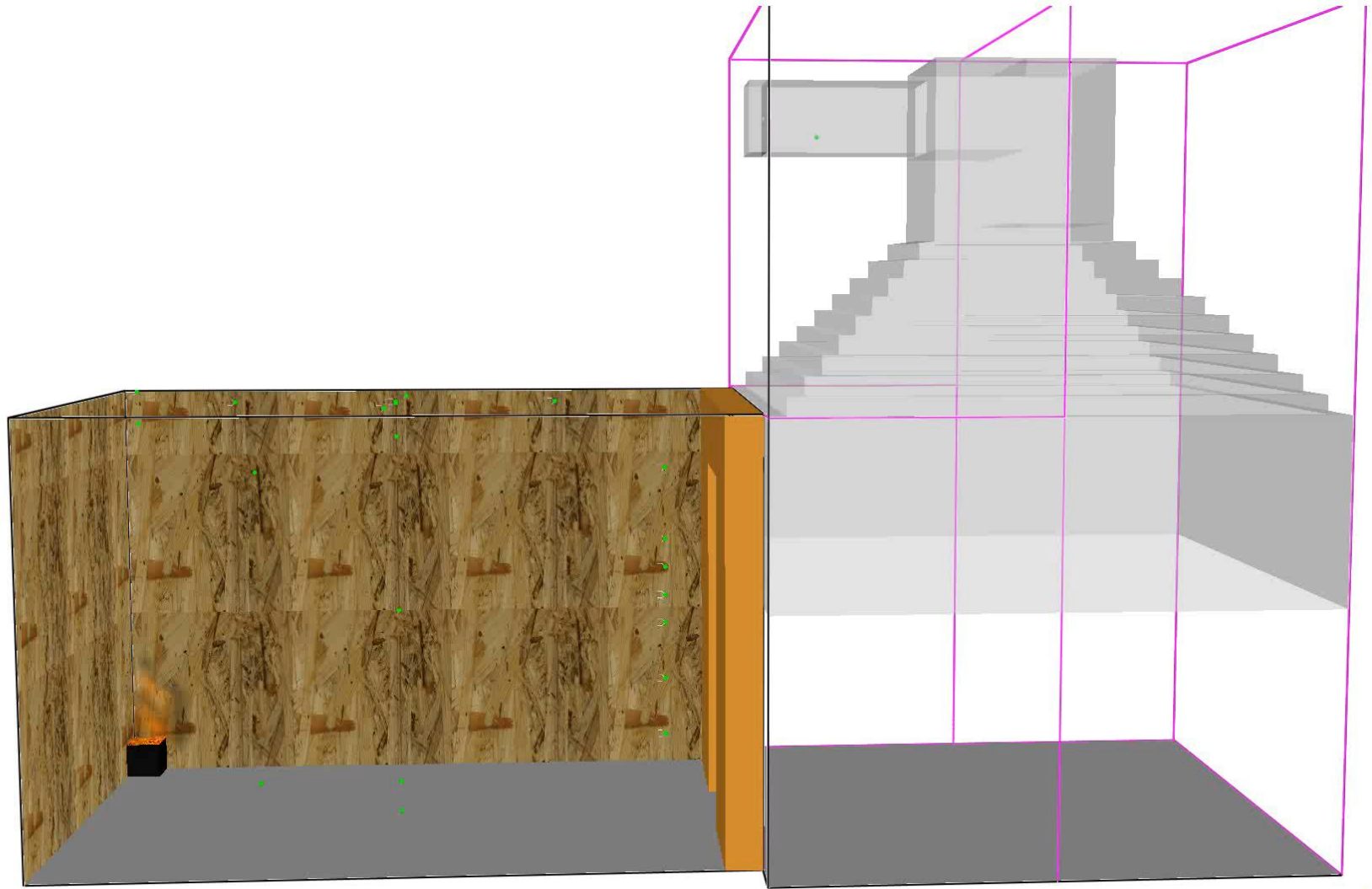
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Reaction to fire tests — Room corner  
test for wall and ceiling lining  
products —

Part 1:  
Test method for a small room  
configuration



# Room Corner Test – FDS model



Frame: 9  
Time: 1.6

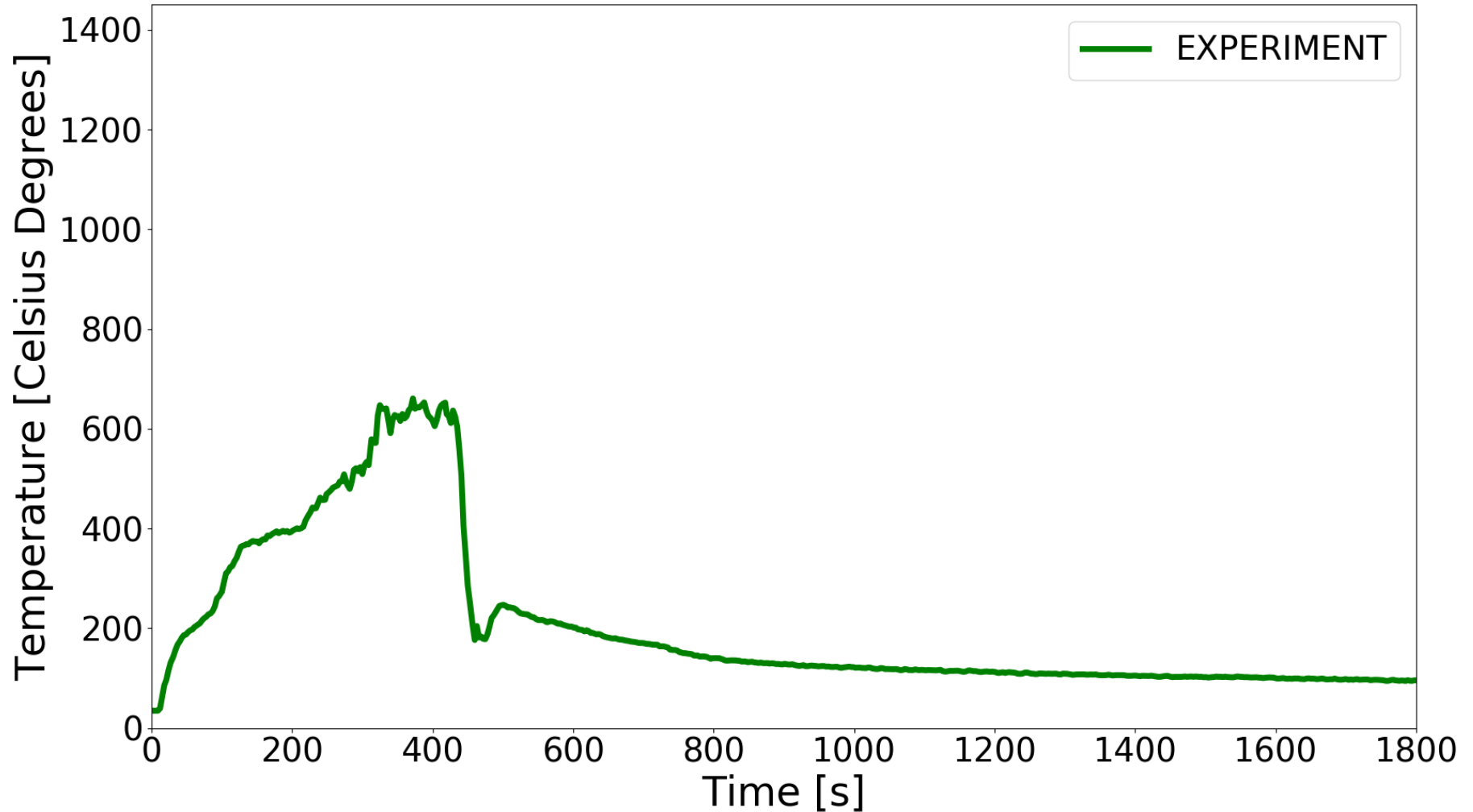
# Investigated Material - OSB

- Engineered/Composite board
- Building material, insulation, interiors
- Charring, inhomogeneous
- Complex chemical structure  
(lignin, cellulose, hemicellulose)  
+ adhesives + additives

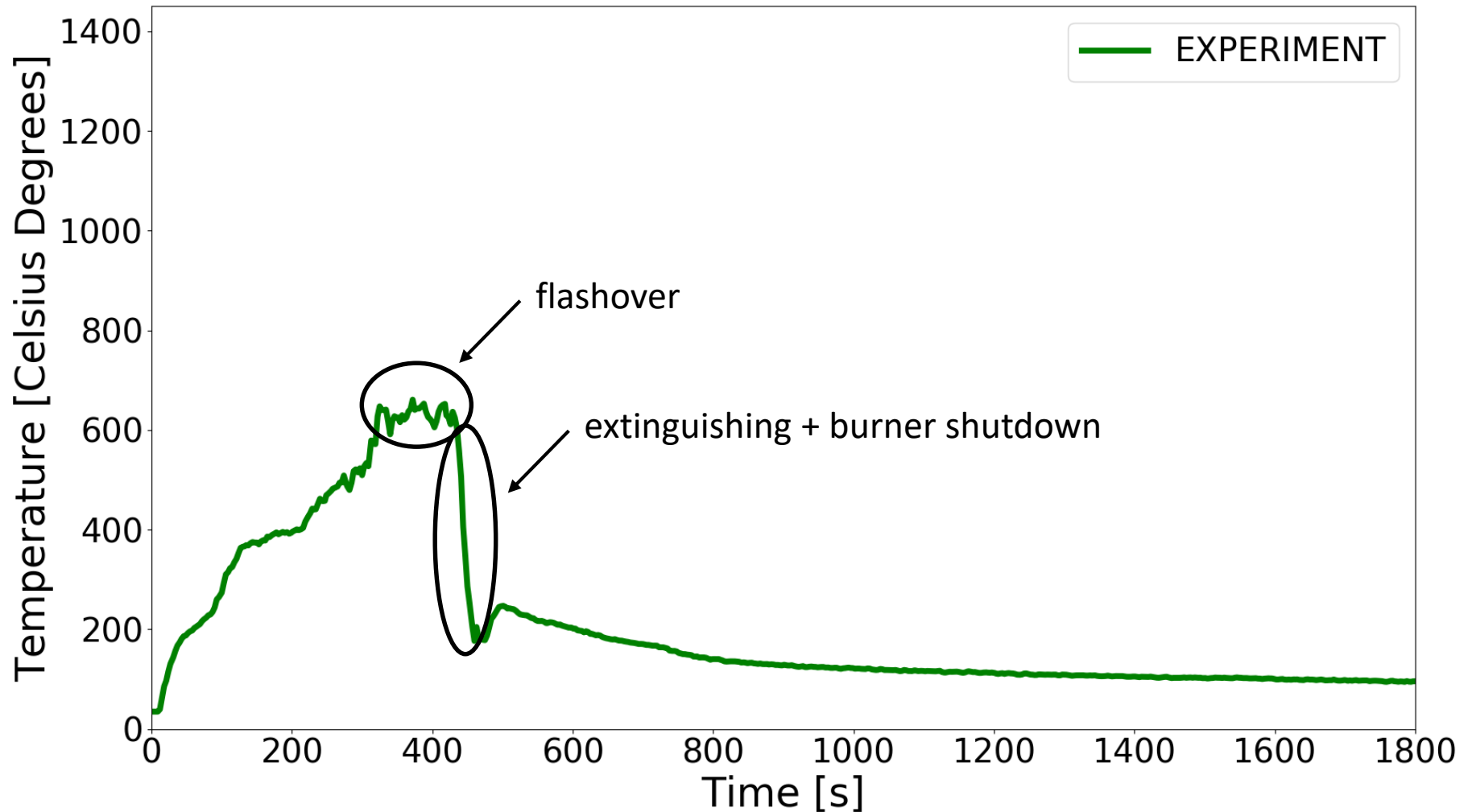




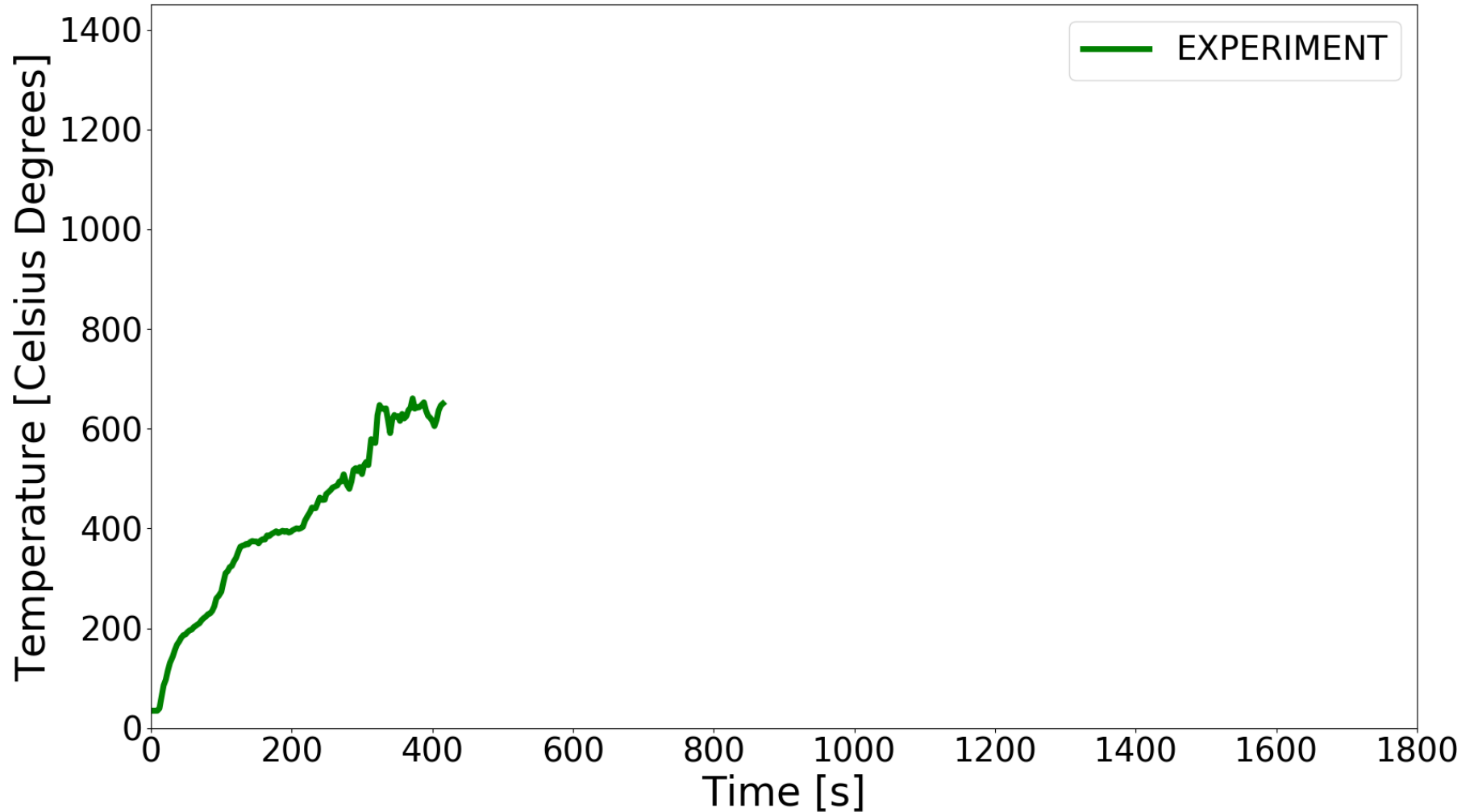
# Experimental Data - Thermocouple



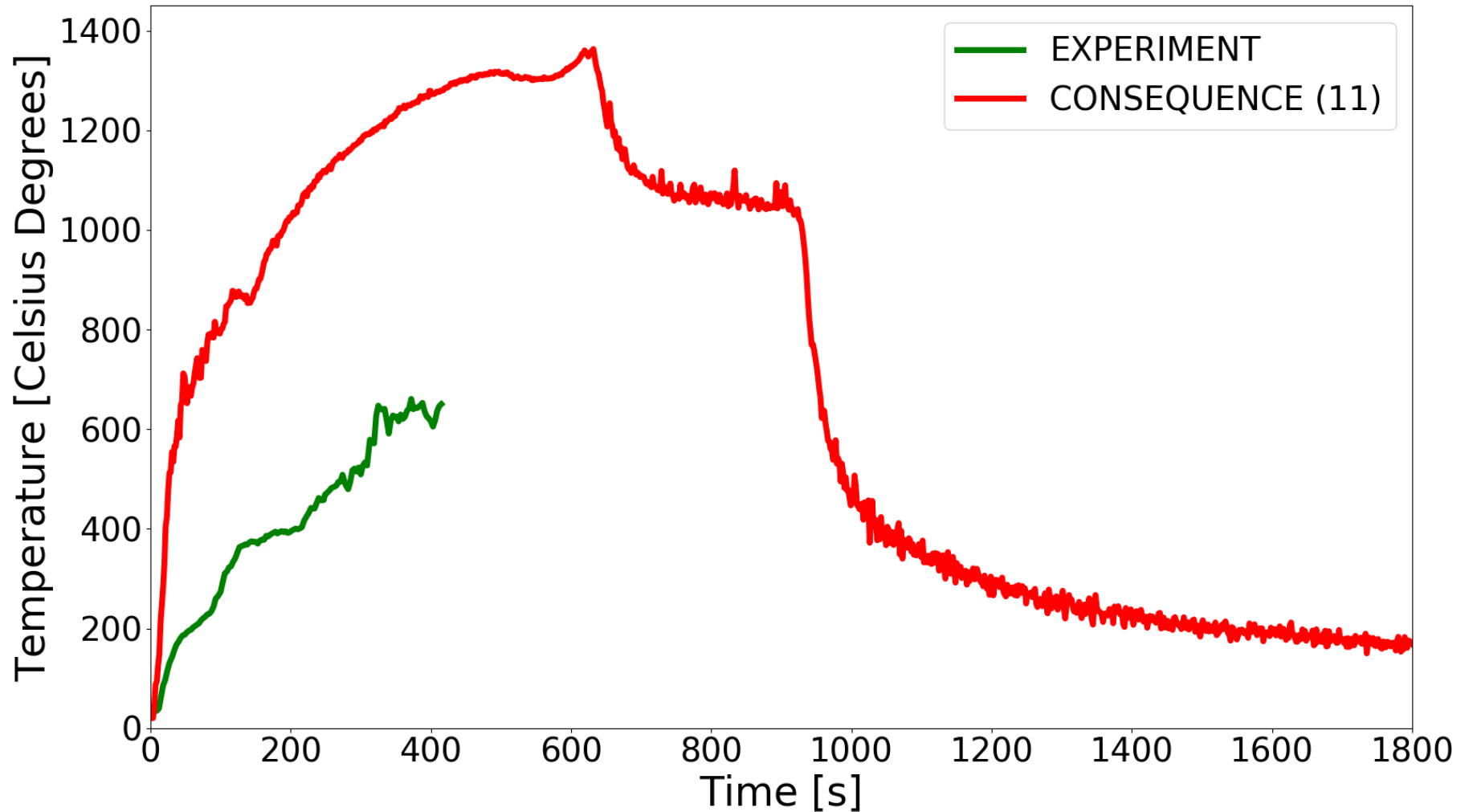
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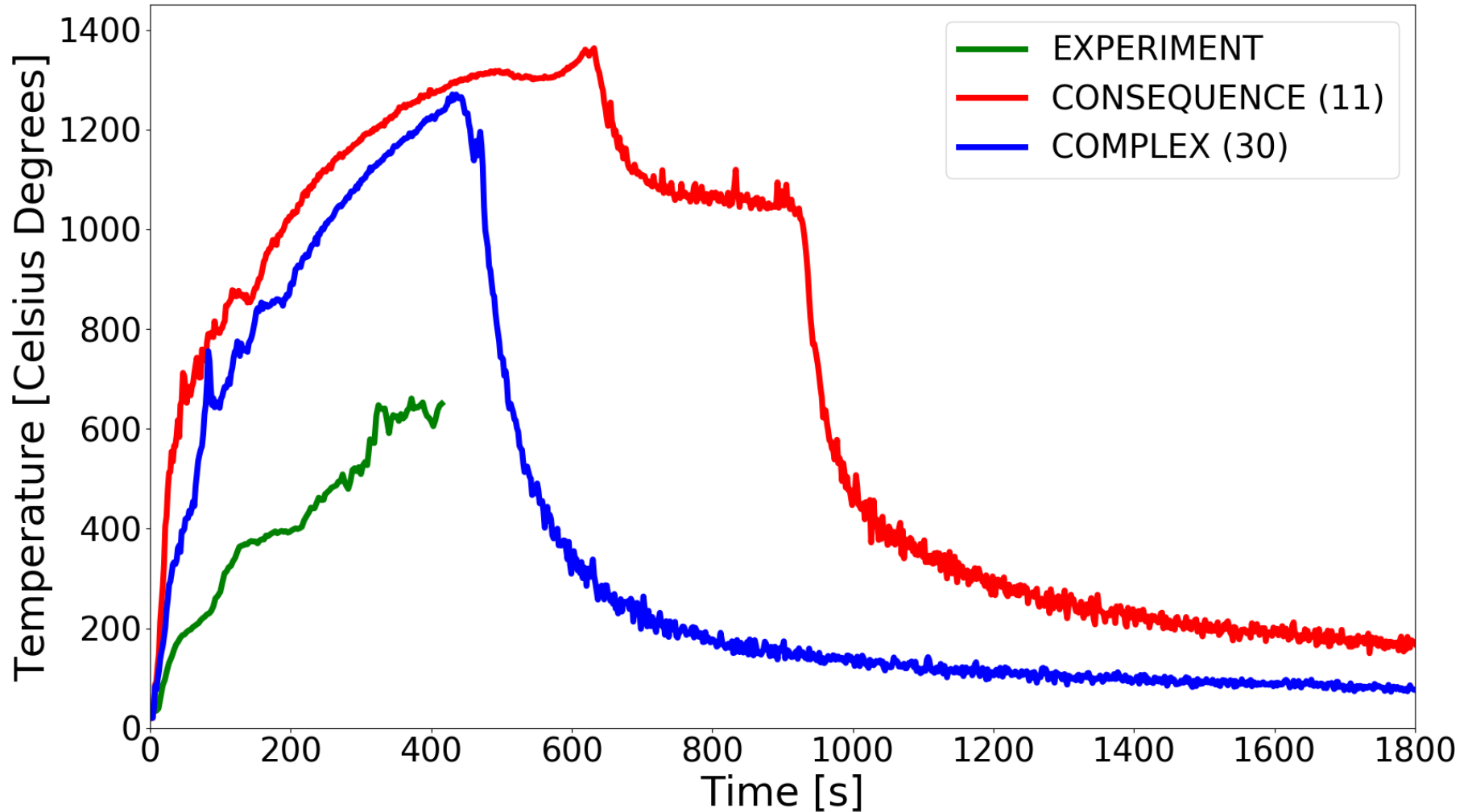
# Experimental Data - Thermocouple



# Experimental Data - Comparison

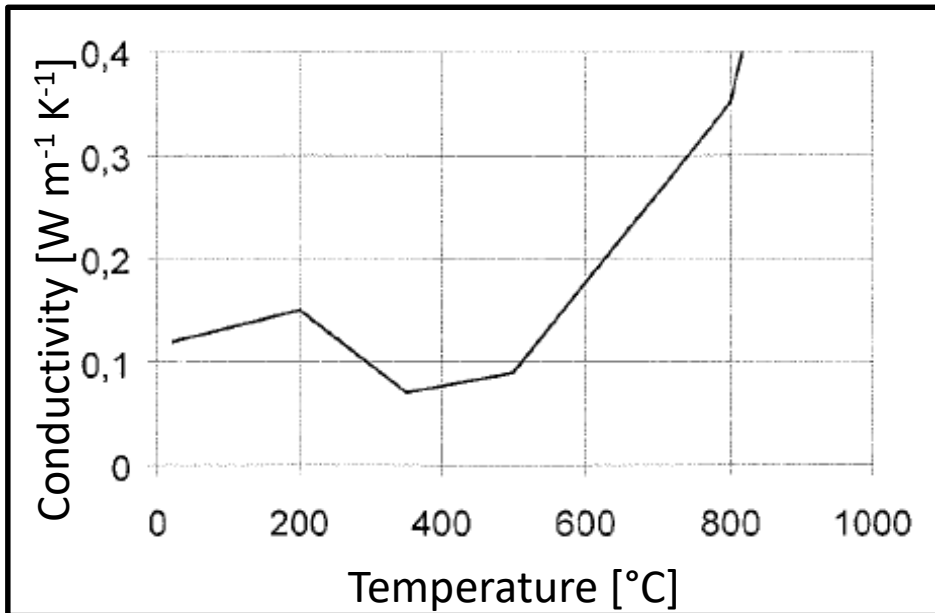
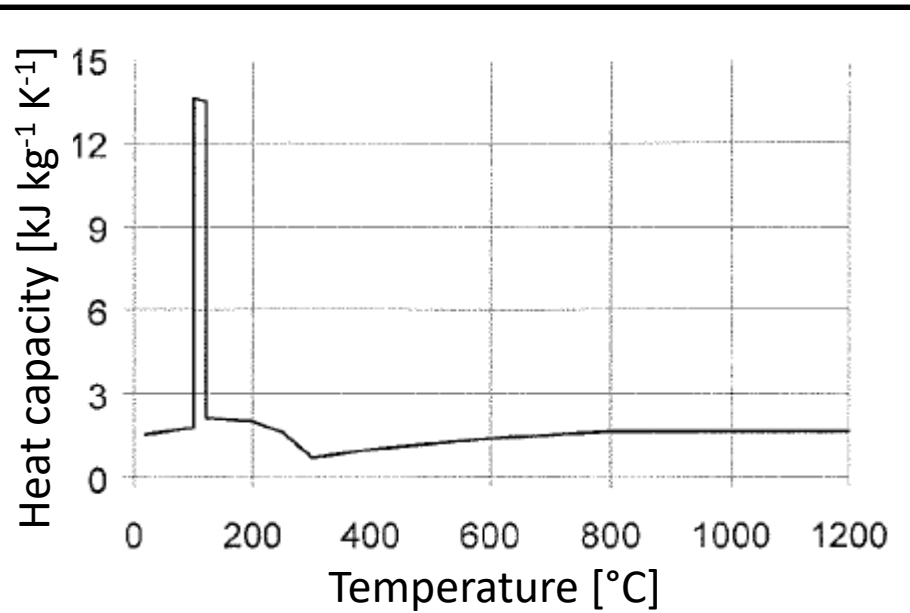


# Experimental Data - Comparison

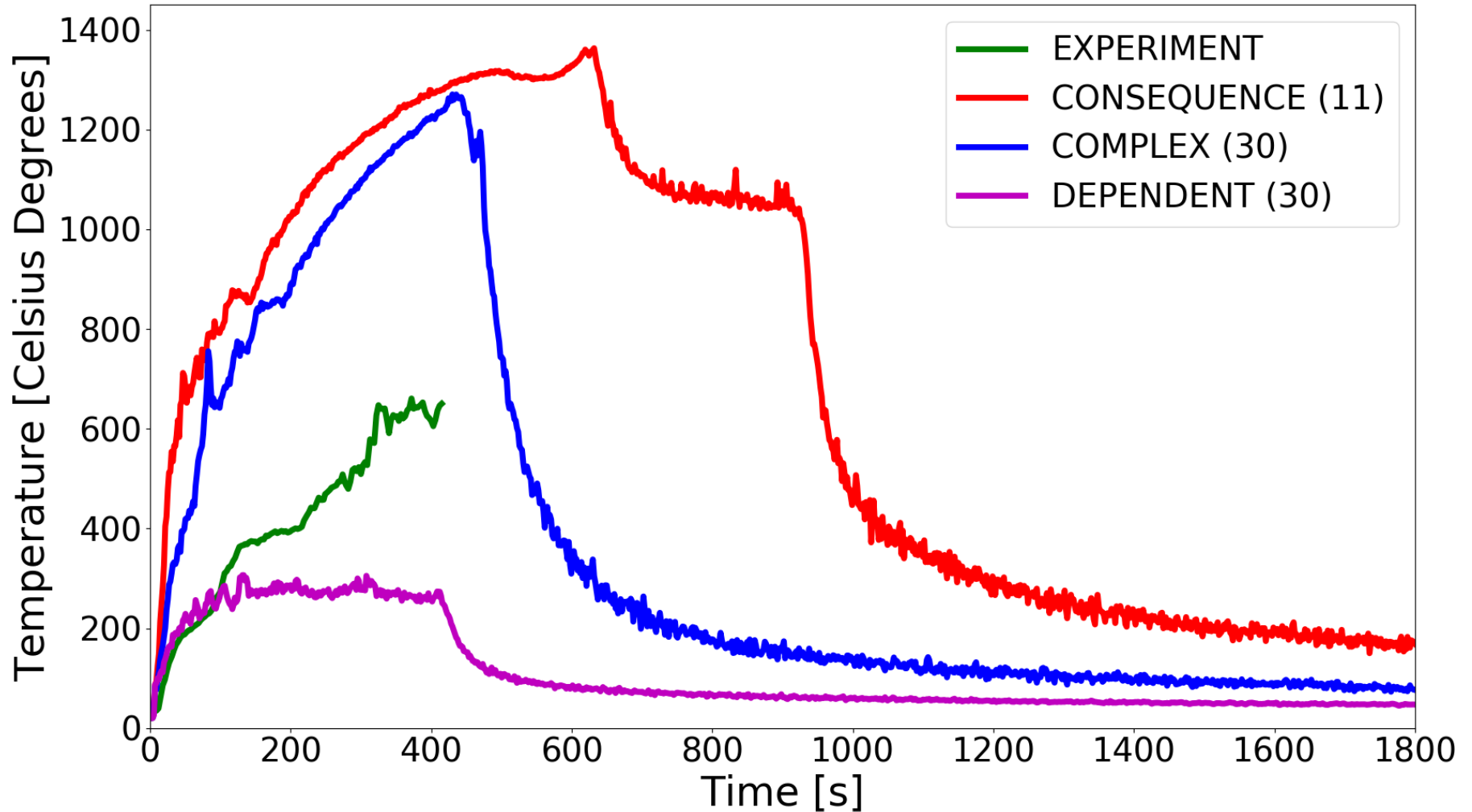


# Temperature Dependent Properties

- Eurocode ČSN EN 1995-1-2

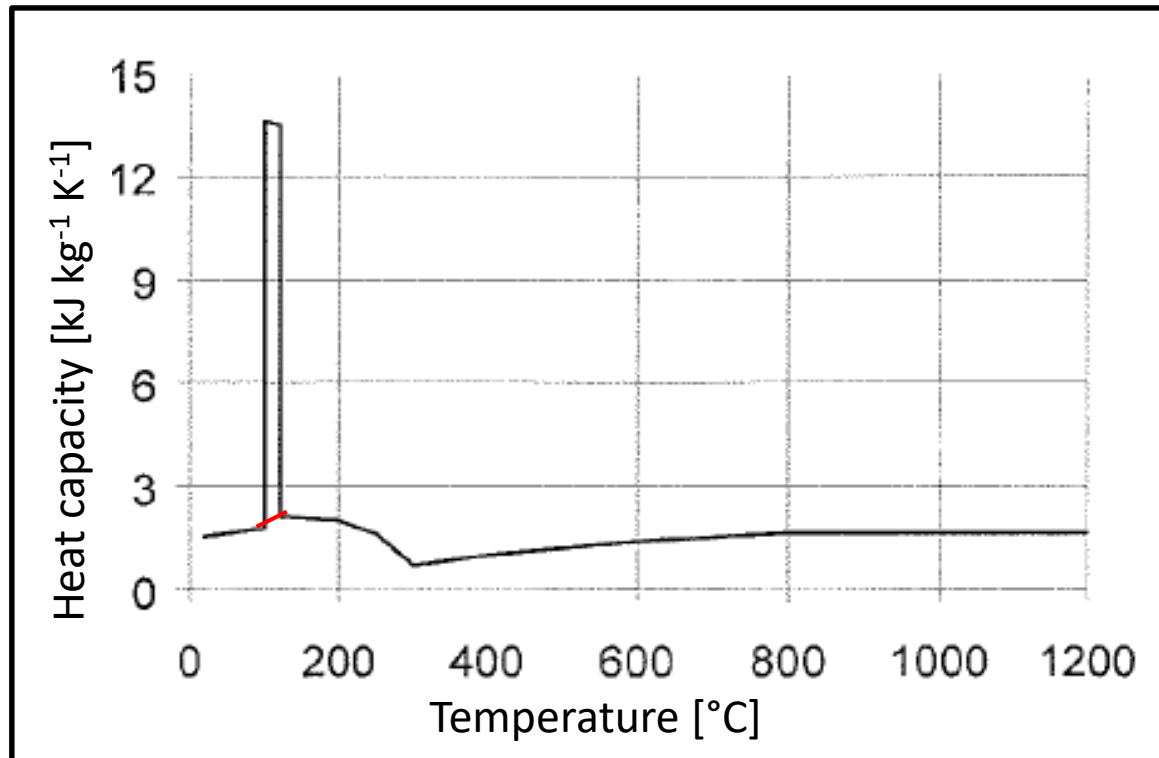


# Experimental Data - Comparison



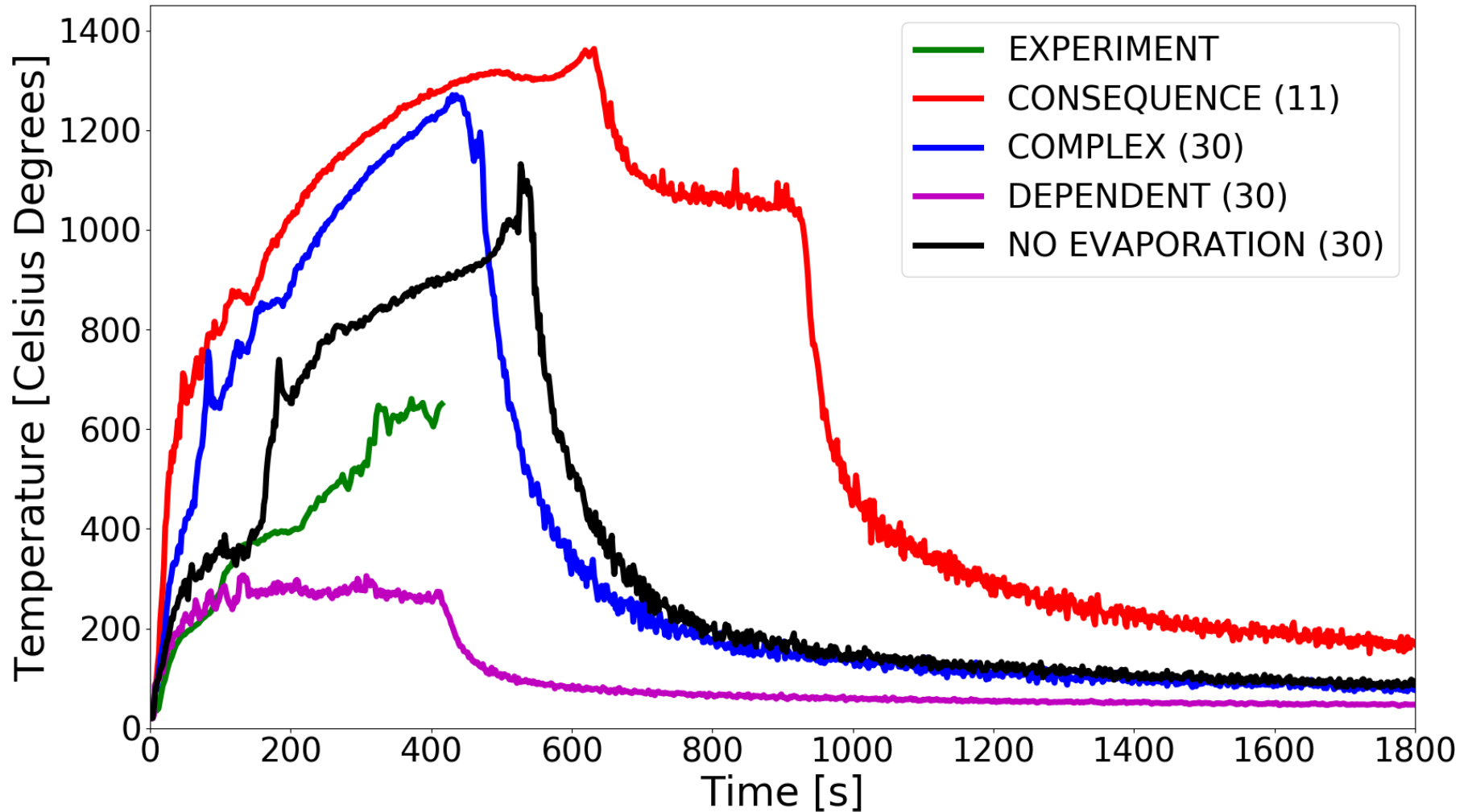
# Temperature Dependent Properties

- Eurocode ČSN EN 1995-1-2
- No evaporation





# Experimental Data - Comparison



# Conclusions and Future Work 2019

- Different pyrolysis models in RCT for OSB board
- HRR modeling insufficient
- Thermal properties most significant
  
- Thermal properties from cone (PROPTI)
- Coupling with structural solvers
- More detailed char analysis

# Conclusions and Future Work 2019

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# New FDS version 6.7.4

- Update from 6.7.1
- Results differ

## FDS 6.7.4 (March 9, 2020)

- Allow particles to follow a `PATH_RAMP(3)` on the `INIT` line; particle `DEVC` output works as usual, so this has the effect of allowing `DEVC` positions to move in time
- Fix bug with FDS+Evac and ZONES
- Fix bug in mass flux of species at exterior boundaries introduced in v6.7.3 for thin obstructions
- Fix bug that prevented defining an `INIT` with a species mass fraction of 0 (i.e. override a non-zero `MASS_FRACTION_0` on `SPEC` ).
- Fix bug in the initialization of pressure at ambient ducts nodes to correctly use the reference elevation.
- Fix bug in the computation of the initial water vapor mass fraction for `HUMIDITY` .
- Fix bug preventing the use of `TMP_INNER` or `RAMP_T_I` for a particle.
- Generalize histogram generation for regular devices.
- Improve `MEAN_FORCING` functionality by averaging velocity over entire domain, not just entire mesh.
- Allow level set wildland fire fronts to cross mesh boundaries.
- Make baroclinic pressure iteration work with GLMAT pressure solver.

# New FDS version 6.7.4

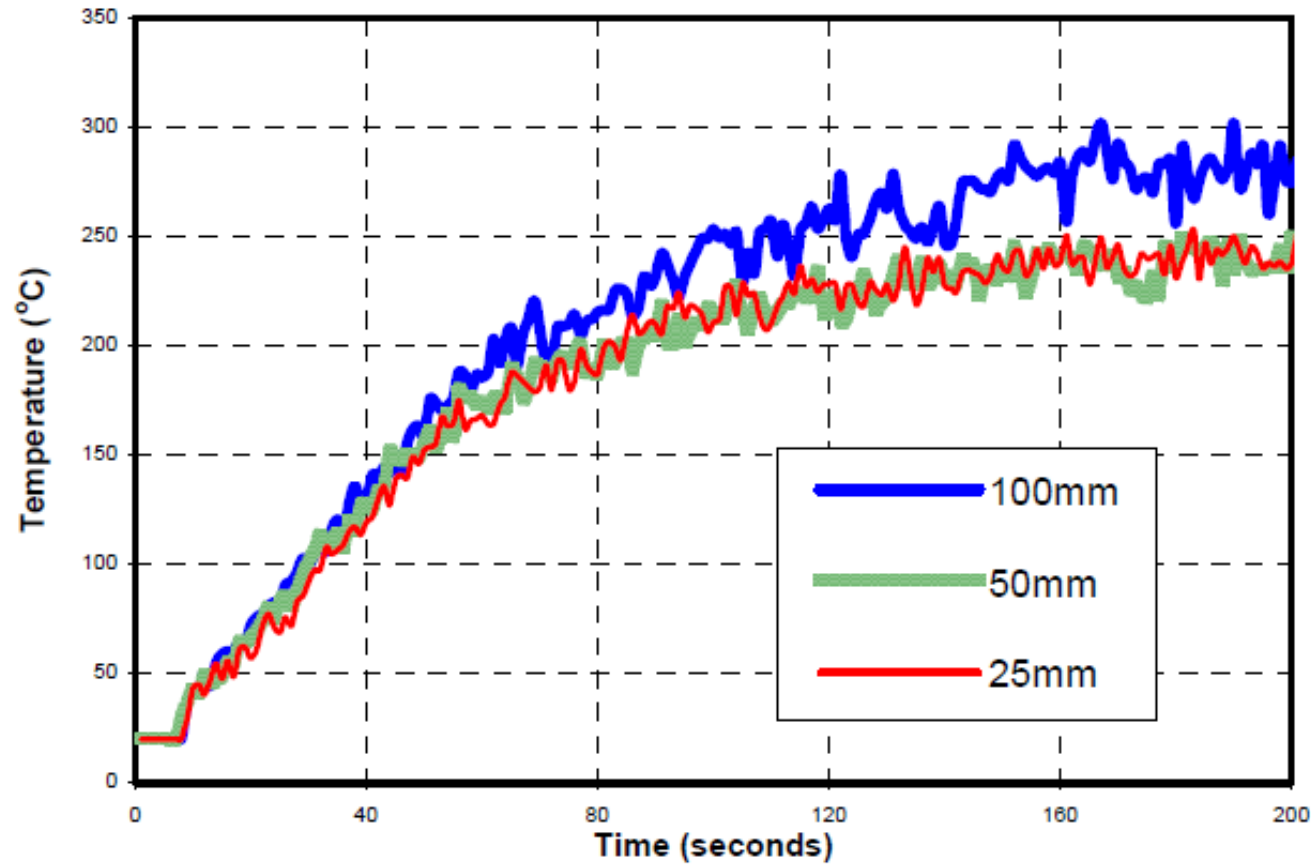
- Solid phase discretization

## FDS 6.7.3 (Oct 31, 2019)

- Allow thin obstructions to burn.
- Force explicit setting of mesh transformation `ID` on `MESH` line via `TRNX_ID`, etc. This allows for much greater flexibility in assigning different transformations to different mesh groups for large-scale calculations.
- `STRETCH_FACTOR` default value set to 2 for all surfaces, even burning surfaces. `STRETCH_FACTOR` controls the size of solid phase cells used to solve the 1-D heat transfer equation.
- Fixed a bug involving pressure `ZONES`. A post to the Forum on June 18th identified a bug where an `OBST` that formed a boundary between two `ZONES` extended over multiple meshes and changed state during the simulation (i.e. had a `CTRL_ID` or `DEVC_ID`). As a result of the bug, the `ZONES` were not properly initialized.
- Fixed a bug in `MIN/MAX CTRL` functions.
- Create a `ZONE` using a single `XYZ` point instead of an `XB` volume spanning multiple meshes.
- Increase length of `FORMULA` (both `REAC` and `SPEC`) to 255 characters
- `PATH_RAMP` on `INIT` can specify a path for a particle.
- Added `HEAT_OF_REACTION_RAMP` to `MATL` to specify a temperature dependent heat of reaction.
- Added `RAMP_T_B` to `SURF` to specify a time dependent back wall gas temperature.

# Gas phase discretization

- Standard procedure
- Adding cells until they affect results



Moghaddam, A. Z., Moinuddin, K., Thomas, I. R., Bennetts, I. D. and Culton, M. (2004) Fire Behaviour Studies of Combustible Wall Linings Applying Fire Dynamics Simulator, 15<sup>th</sup> Australasian Fluid Mechanics Conference.



# Solid phase discretization

- Need to solve partial differential equations for heat conduction

$$\rho_s c_s \frac{\partial T_s}{\partial t} = \frac{\partial}{\partial x} \left( k_s \frac{\partial T_s}{\partial x} \right) + \dot{q}_s'''$$

$$-k_s \frac{\partial T_s}{\partial x}(0,t) = \dot{q}_c'' + \dot{q}_r''$$

$$\frac{T_{s,i}^{n+1} - T_{s,i}^n}{\delta t}$$



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$$\frac{T_{s,i}^{n+1} - T_{s,i}^n}{\delta t}$$

- Crank-Nicolson scheme (implicit)

$$\begin{aligned} (\rho_s c_s)_i \frac{T_{s,i}^{n+1} - T_{s,i}^n}{\delta t} &= \frac{1}{2r_{c,i}^J \delta r_i} \left( r_i^J k_{s,i+\frac{1}{2}} \frac{T_{s,i+1}^n - T_{s,i}^n}{\delta r_{i+\frac{1}{2}}} - r_{i-1}^J k_{s,i-\frac{1}{2}} \frac{T_{s,i}^n - T_{s,i-1}^n}{\delta r_{i-\frac{1}{2}}} \right) \\ &+ \frac{1}{2r_{c,i}^J \delta r_i} \left( r_i^J k_{s,i+\frac{1}{2}} \frac{T_{s,i+1}^{n+1} - T_{s,i}^{n+1}}{\delta r_{i+\frac{1}{2}}} - r_{i-1}^J k_{s,i-\frac{1}{2}} \frac{T_{s,i}^{n+1} - T_{s,i-1}^{n+1}}{\delta r_{i-\frac{1}{2}}} \right) + \dot{q}_{s,i}''' \end{aligned}$$

# Solid phase discretization

- Need to solve partial differential equations for heat conduction

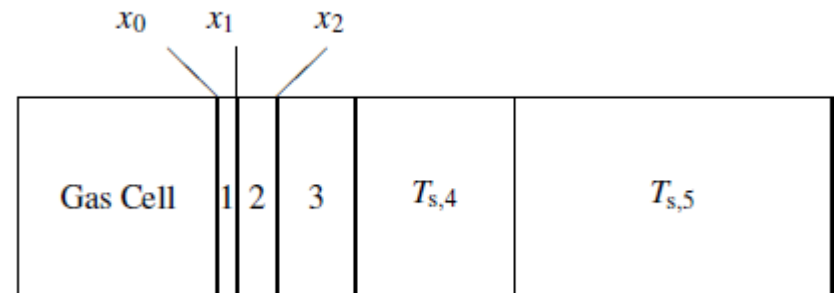
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$$\frac{T_{s,i}^{n+1} - T_{s,i}^n}{\delta t}$$

- Default discretization:

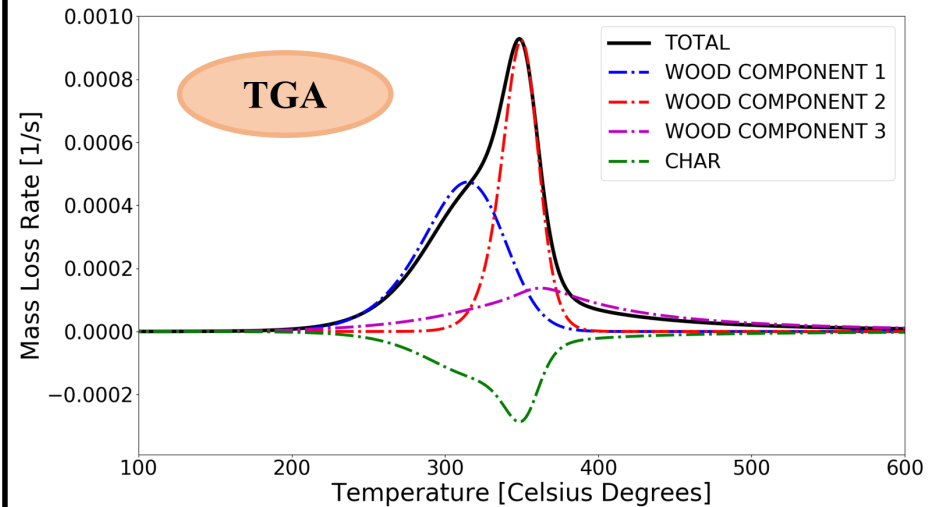
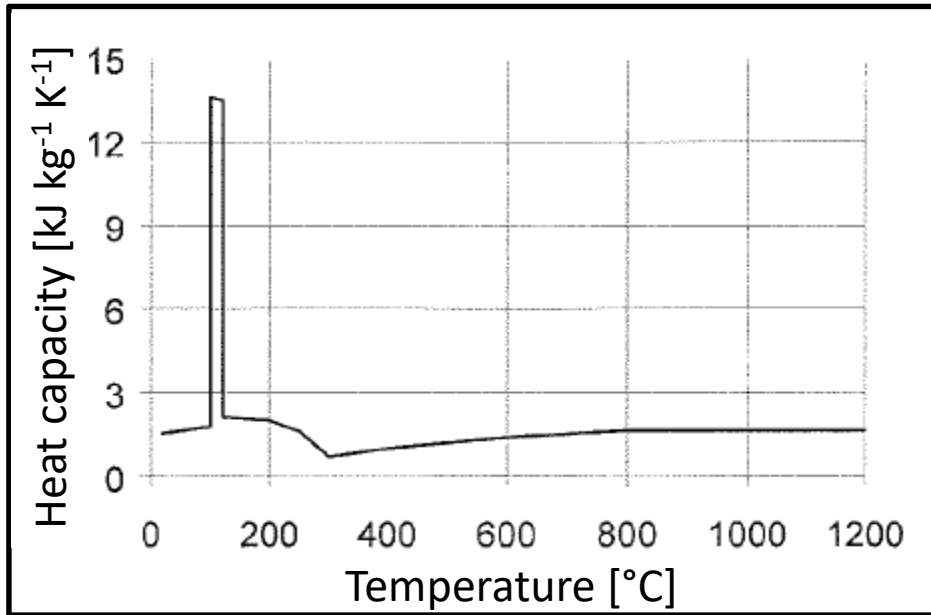
- Wall increment = 2
- Stretch factor = 2
- First cell size  $\leq \sqrt{tk_s/\rho c_s}$
- Cell size factor = 1



- Why is default not sufficient?

# Why is the default not sufficient?

- Reaction rate! (3 pyrolysis reactions)
- Temperature dependent properties



# Solid phase discretization

- Need to solve partial differential equations for heat conduction

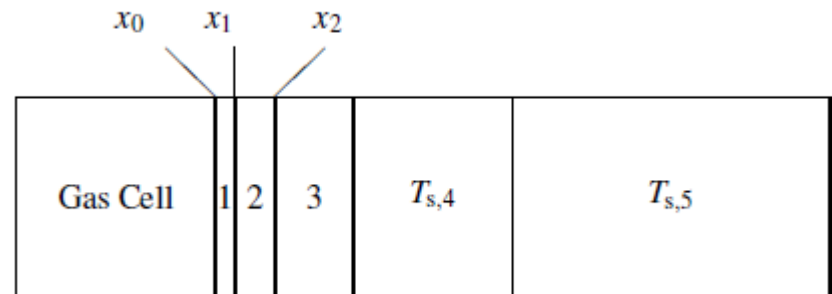
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$$\frac{T_{s,i}^{n+1} - T_{s,i}^n}{\delta t}$$

- Default discretization:

- Wall increment = 2
- Stretch factor = 2
- First cell size  $\leq \sqrt{tk_s/\rho c_s}$
- Cell size factor = 1

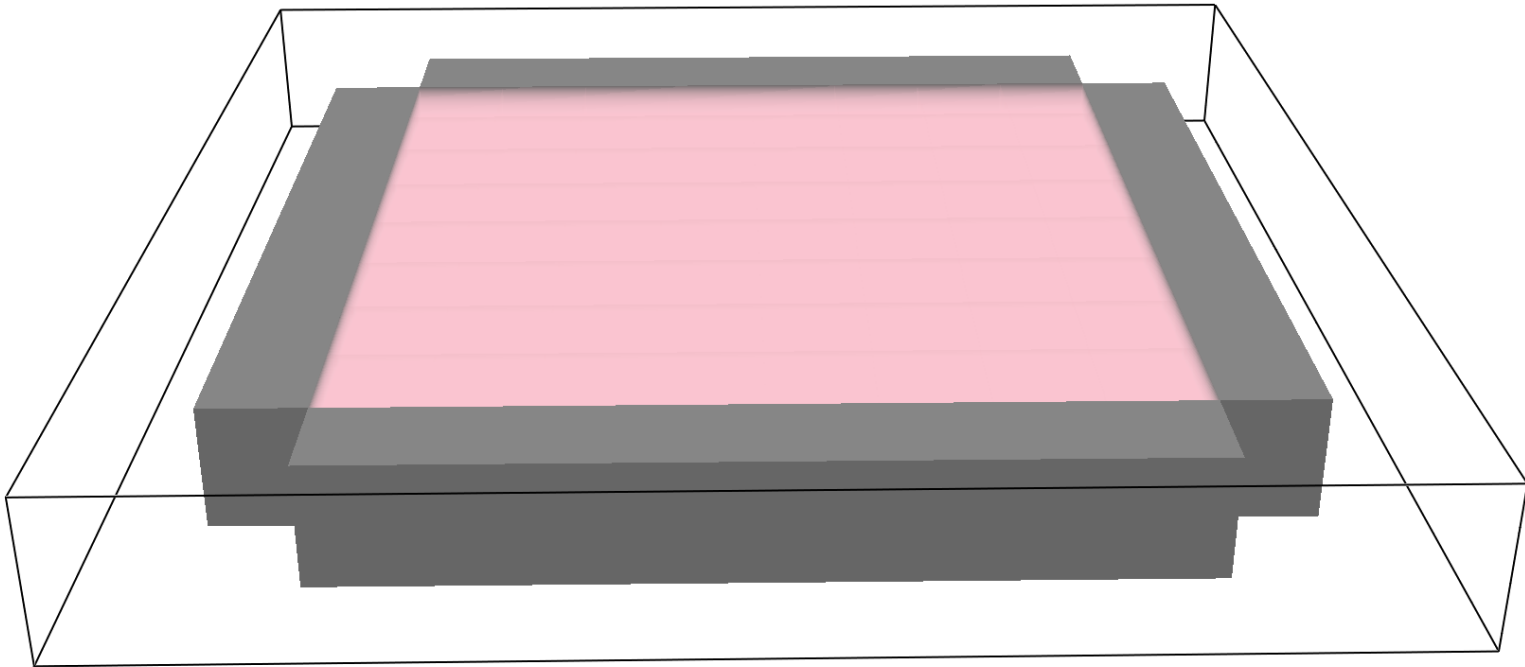


- **Adjusted discretization:**

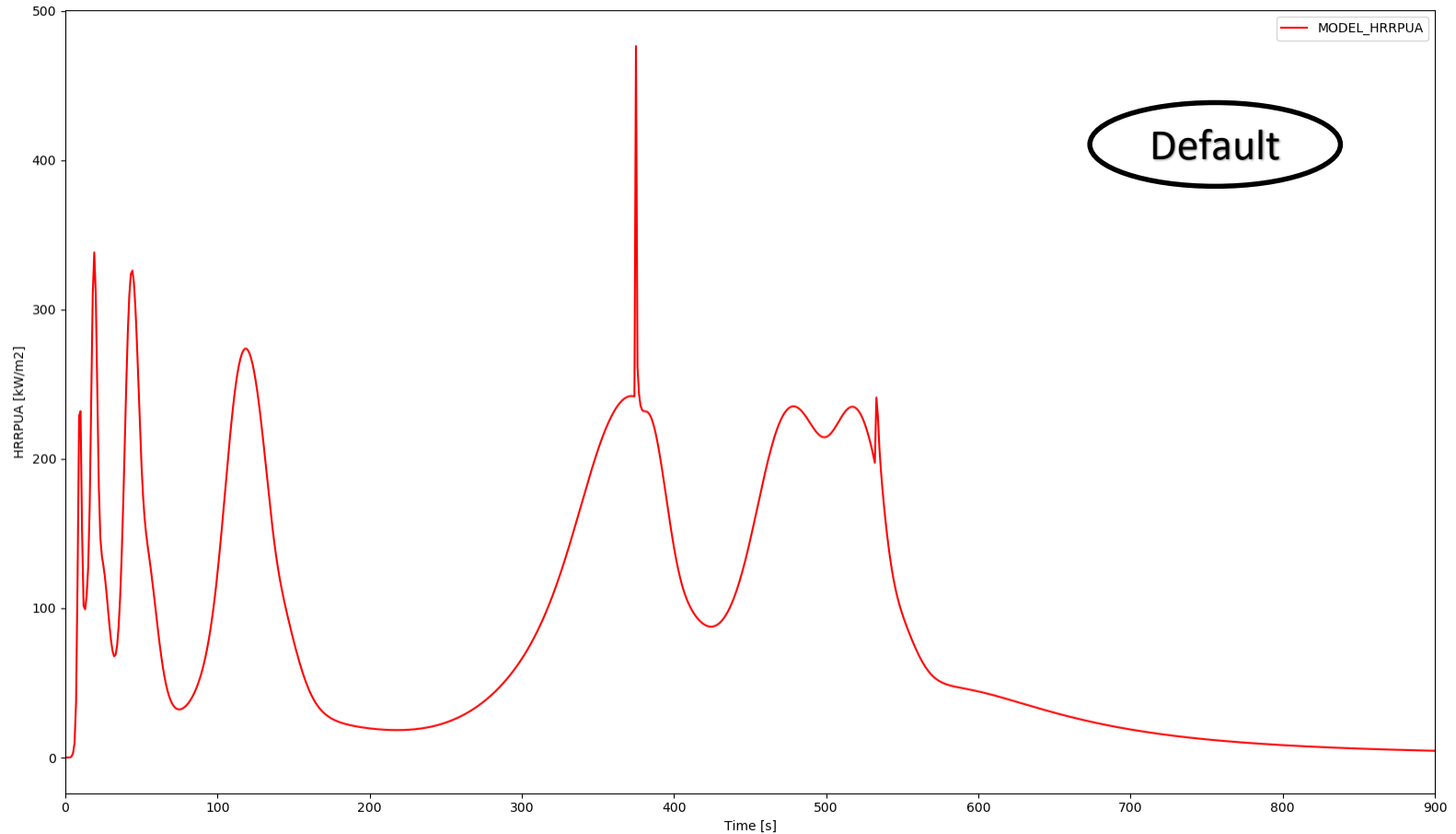
- **Wall increment = 1**
- **Stretch factor = 1**
- **Cell size factor < 1**
- **Large increase in computational time**

# Solid phase discretization

- Inappropriate to observe solid phase discretization effect from large scale models and from gas phase cells properties
- Focus only on solid phase (solid phase only = true) -> Cone
- Simplest geometry possible

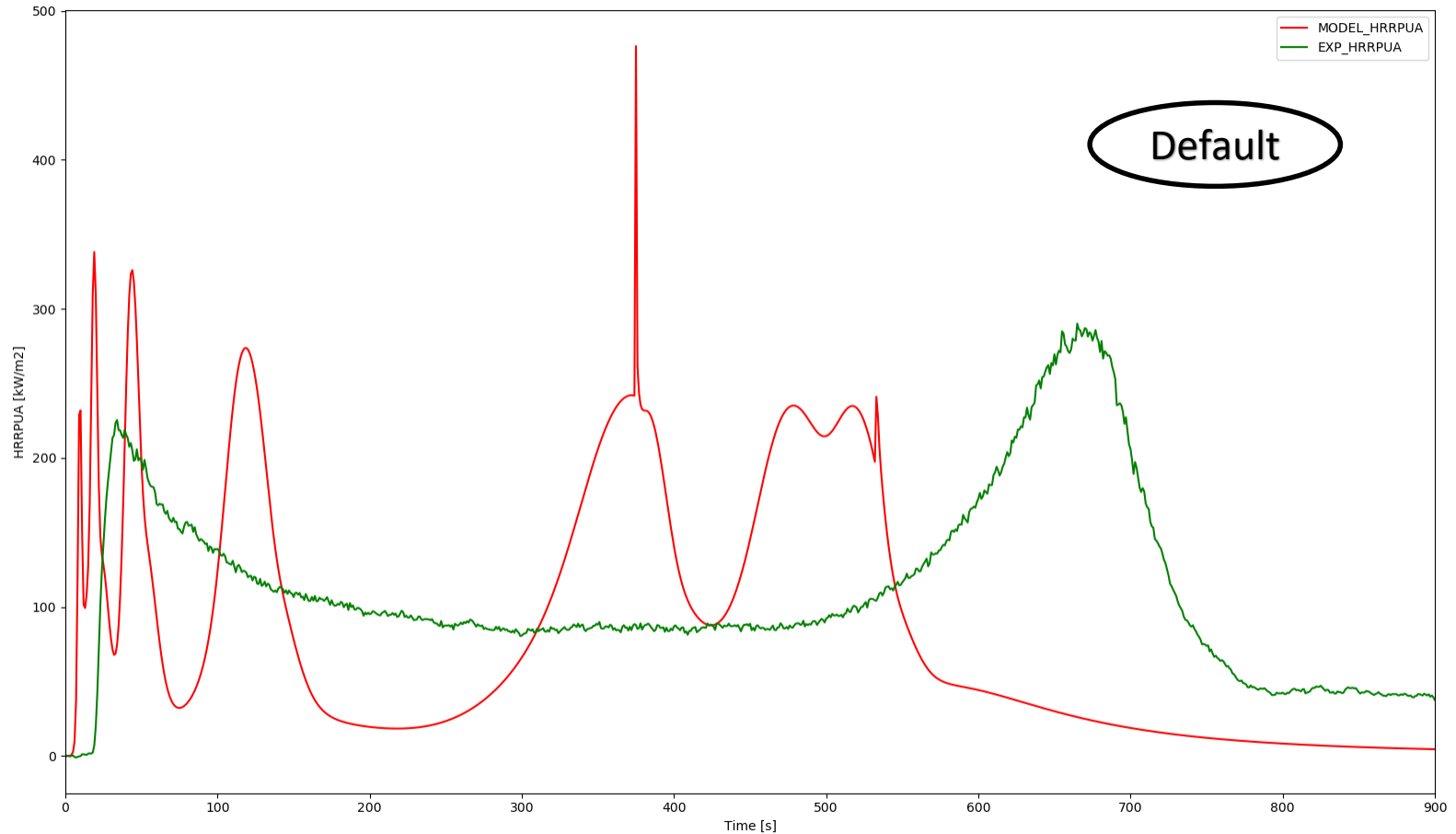


# FDS cone calorimetry model



- 50 kW
- 6 sec, 10 cells

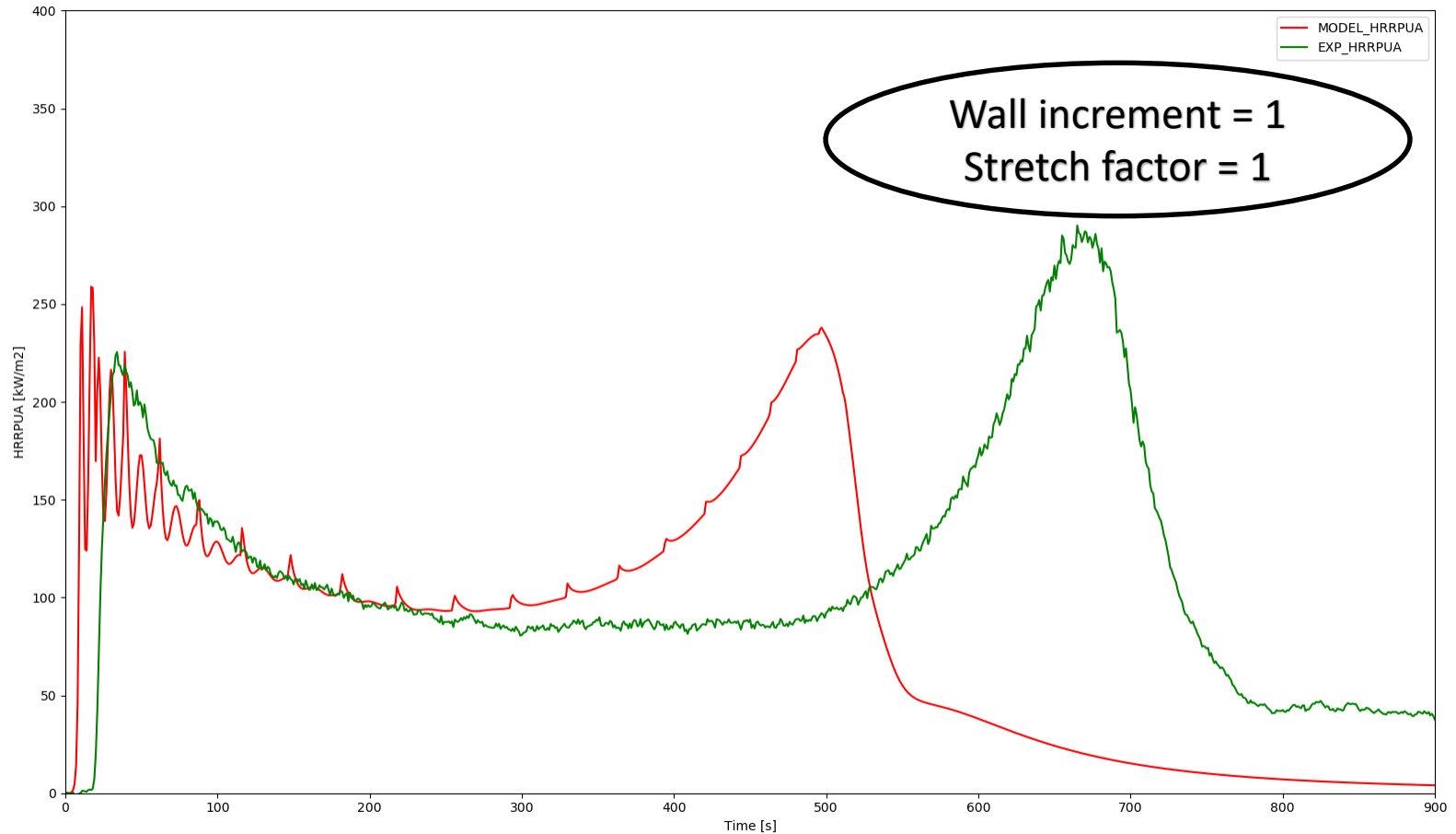
# FDS cone calorimetry model



- 50 kW
- 6 sec, 10 cells

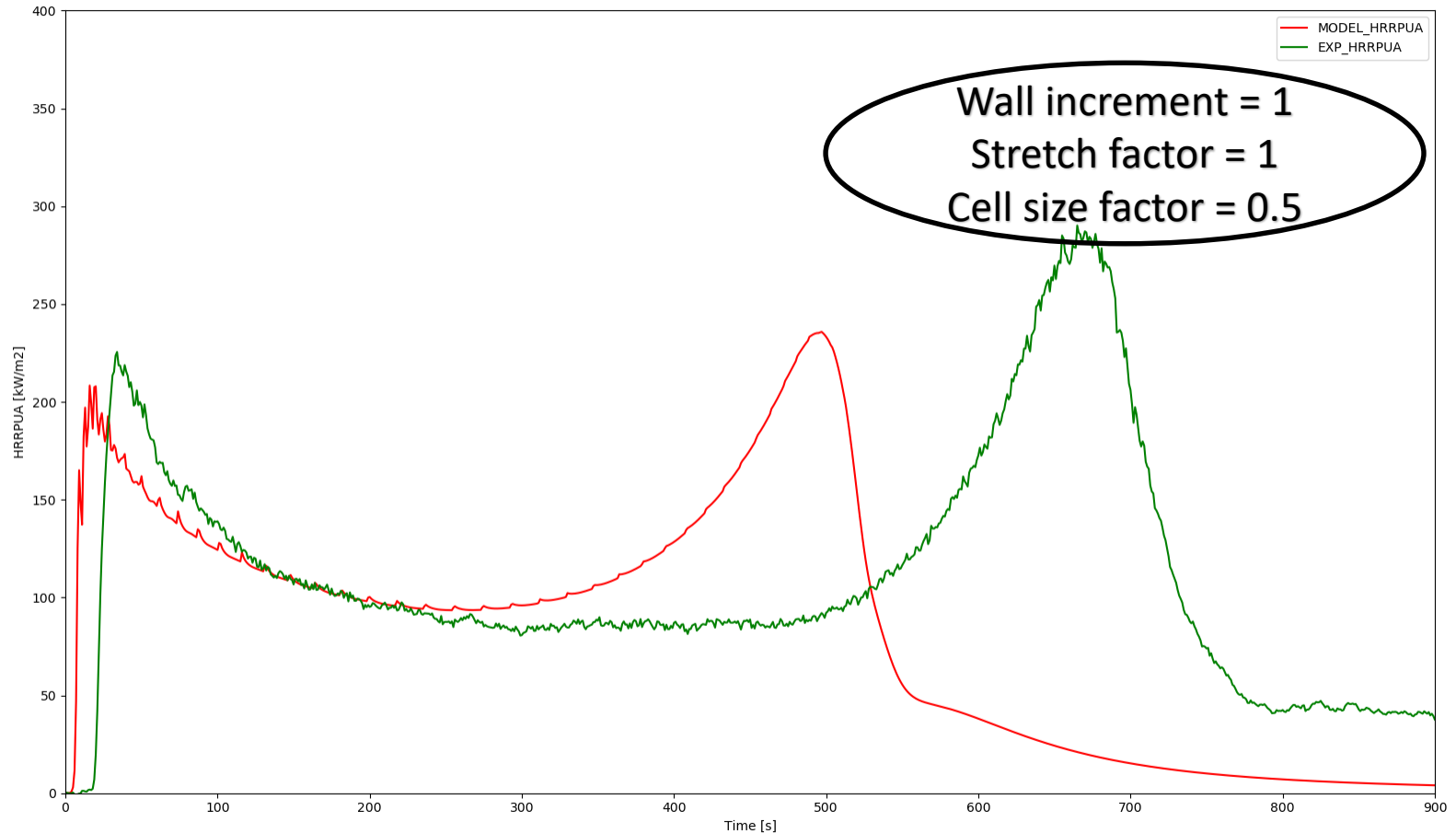


# FDS cone calorimetry model



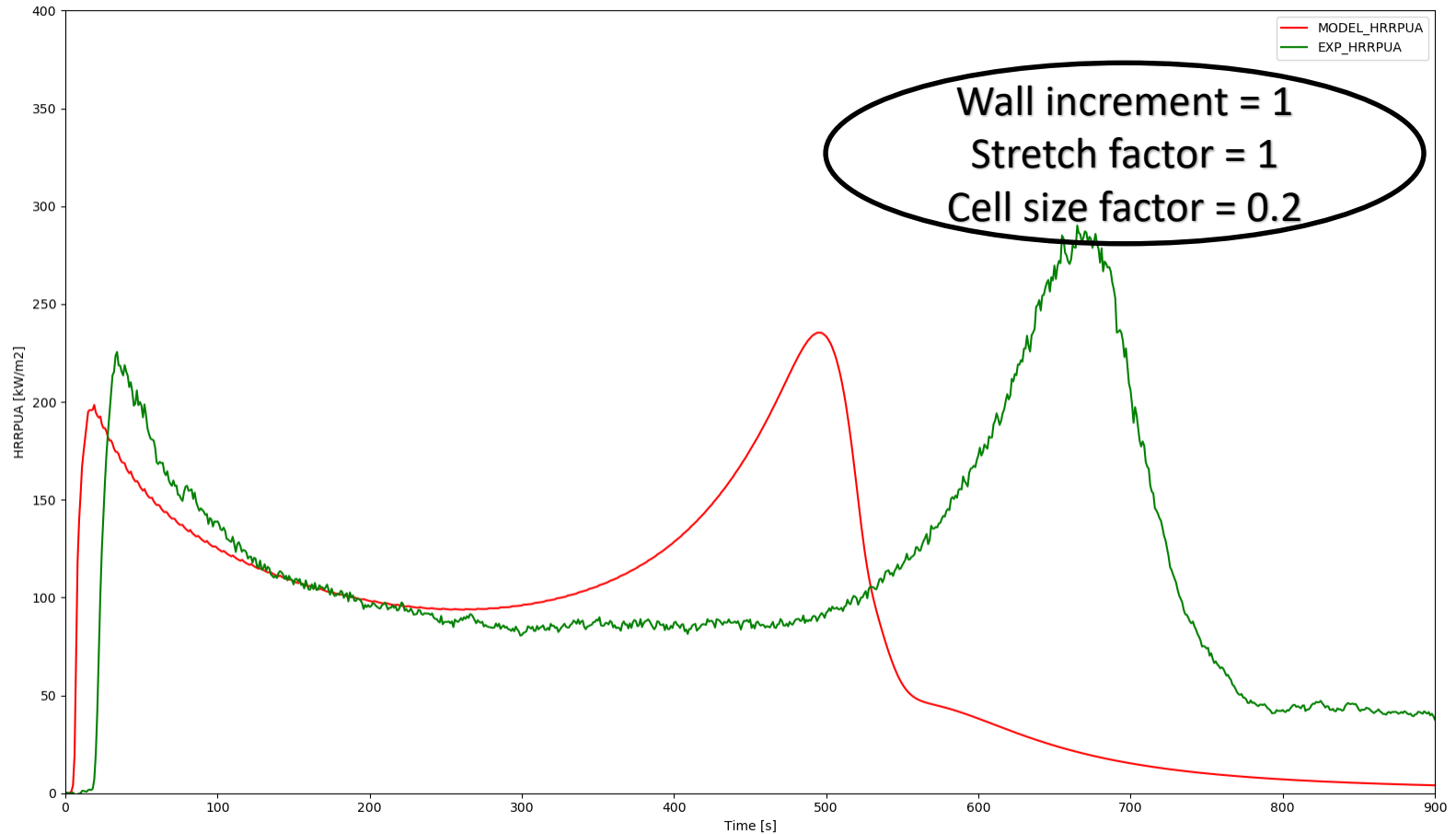
- 50 kW
- 7 sec, 42 cells

# FDS cone calorimetry model



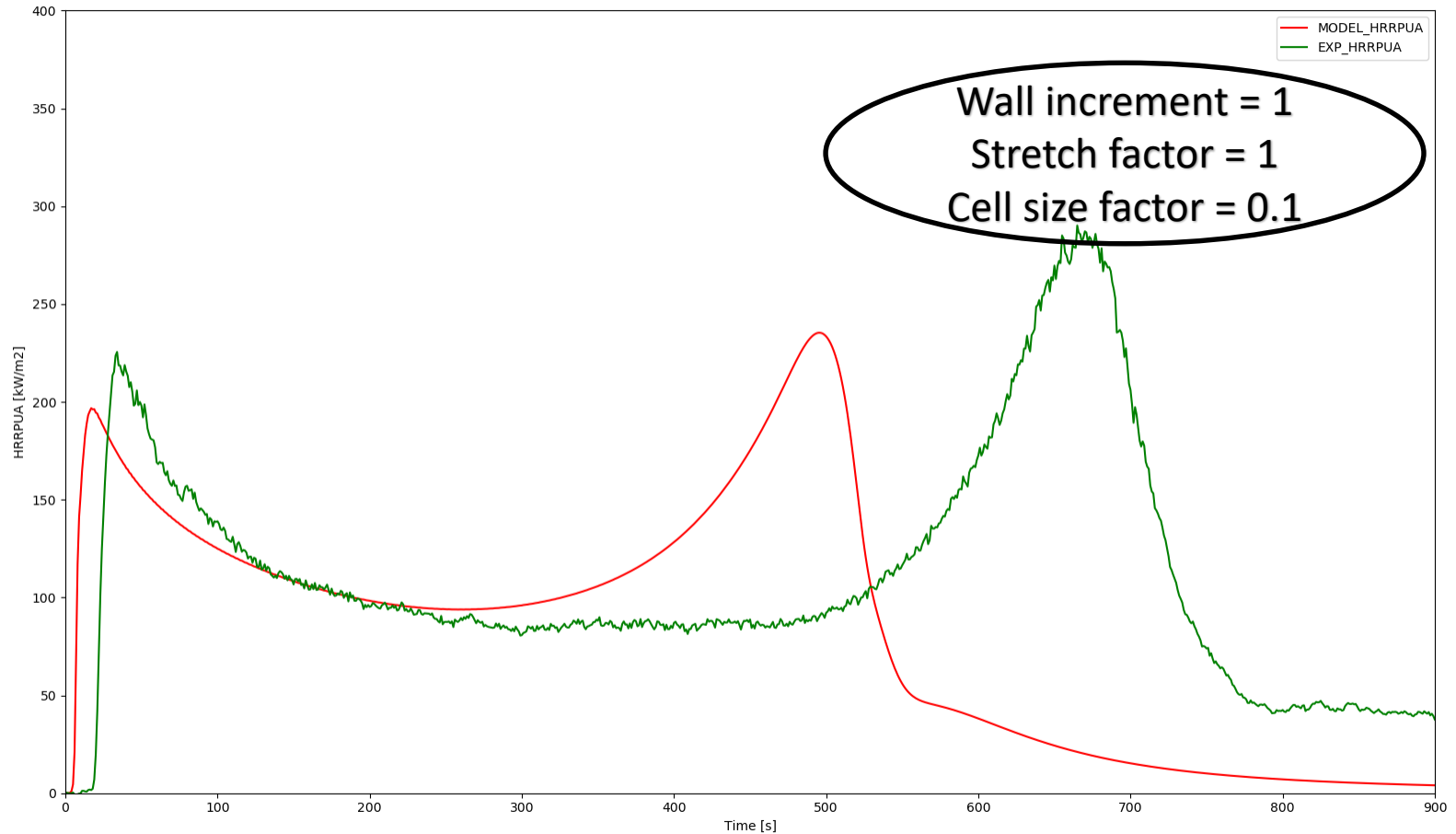
- 50 kW
- 8 sec, 83 cells

# FDS cone calorimetry model



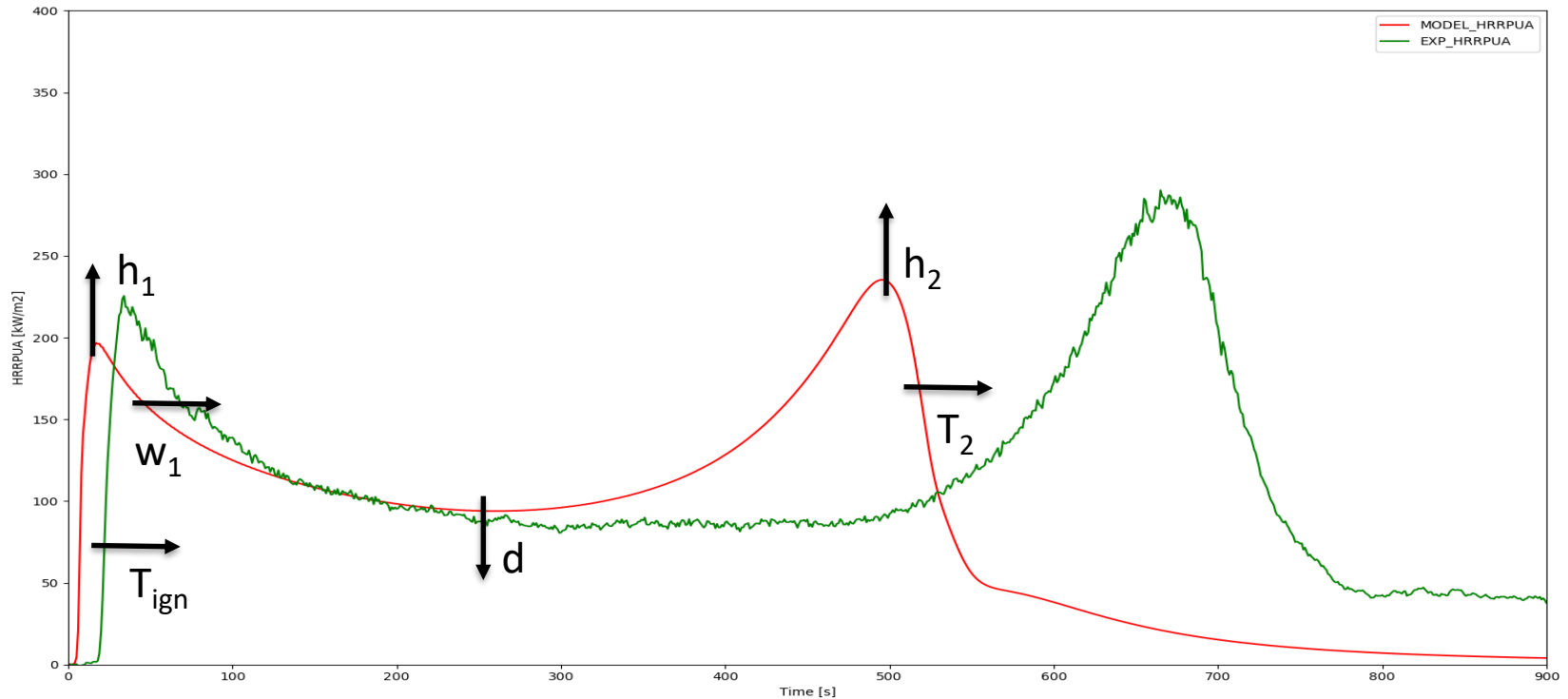
- 50 kW
- 15 sec, 204 cells

# FDS cone calorimetry model



- 50 kW
- 42 sec, 407 cells

# FDS cone calorimetry model



Effect	$k_{solid}$	$c_{p,solid}$	$k_{char}$	$c_{p,char}$	$\Delta H$	$\Delta H_c$
Time of ignition ( $T_{ign}$ )	+	+	0	0	0	0
1st peak (width) ( $w_1$ )	0	0	+	0	(-)	0
1st peak (height) ( $h_1$ )	0	0	0	0	(-)	+
Depth of valley ( $d$ )	0	+	-	0	+	+
2nd peak (time) ( $T_2$ )	-	+	-	0	0	+
2nd peak (height) ( $h_2$ )	+	+	+	-	-	+

# FDS - PROPTI cone calorimetry model

- Optimization, analogy to kinetics from TGA data
- Selection of searched parameters
  - $c_s$  of char <0.2; 2.0> (literature 0.8)
  - $k_s$  of char <0.02; 0.3> (literature 0.1)
  - $c_s$  of all 3 wood components <0.3; 3> (literature 1.221)
  - $k_s$  of all 3 wood components <0.02; 0.3> (literature 0.098)

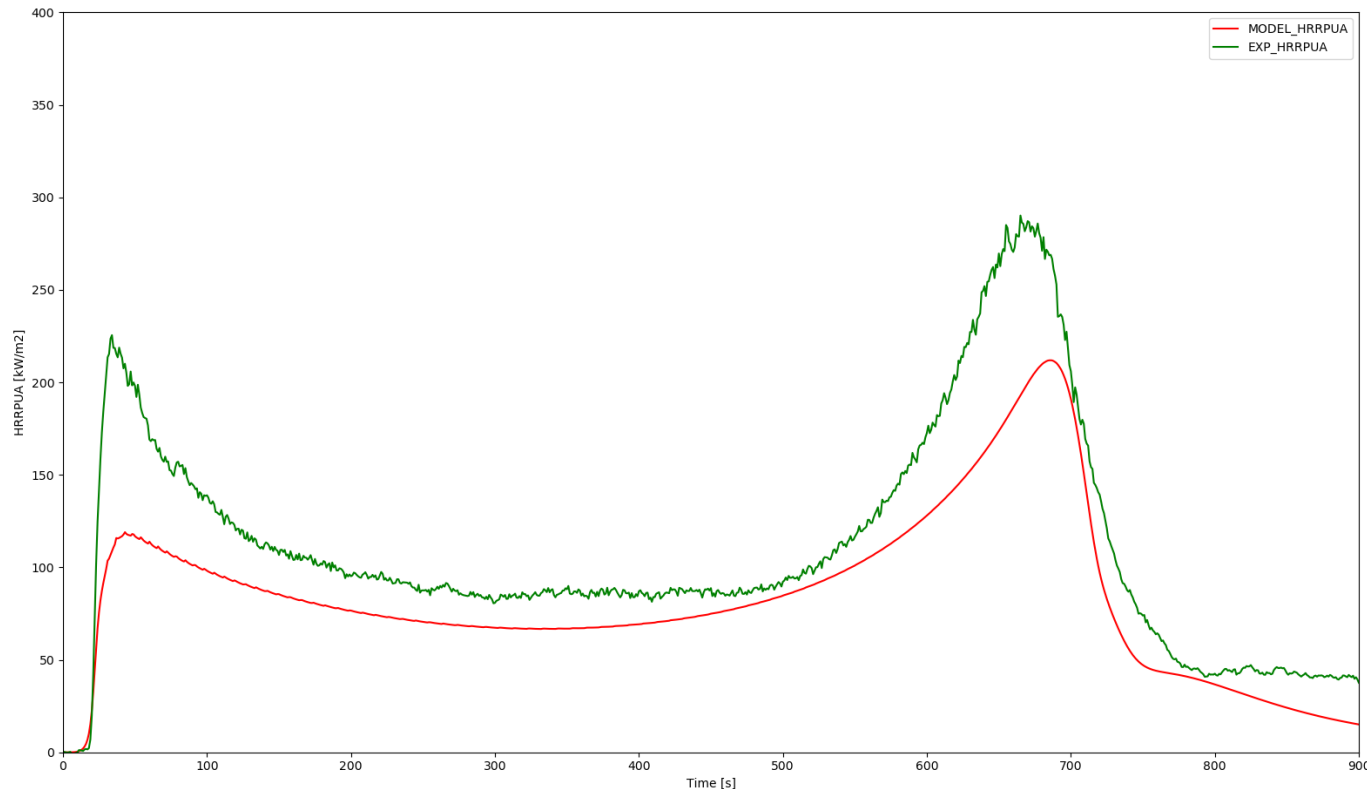
```
&MATL ID='LIGNIN',  
  SPECIFIC_HEAT=#Cp_01#,  
  CONDUCTIVITY=#K_01#,  
  DENSITY=587.1,  
  N_REACTIONS=1.,  
  A(1)=38018940.,  
  E(1)=112460.,  
  N_S(1)=1.21,  
  MATL_ID(1,1)='CHAR',  
  NU_MATL=0.2306,  
  SPEC_ID(1,1)='REAC_FUEL',  
  NU_SPEC(1,1)=0.7694,  
  HEAT_OF_REACTION=77.7,  
  HEAT_OF_COMBUSTION=11710. /
```

```
&MATL ID='CHAR',  
  SPECIFIC_HEAT=#Cp_CH#,  
  CONDUCTIVITY=#K_CH#,  
  DENSITY=299.0/
```

```
# use default values for optimiser  
optimiser = pr.OptimiserProperties(algorithm='sceua',  
                                   repetitions=10000,  
                                   ngs=4,  
                                   backup_every=100)
```

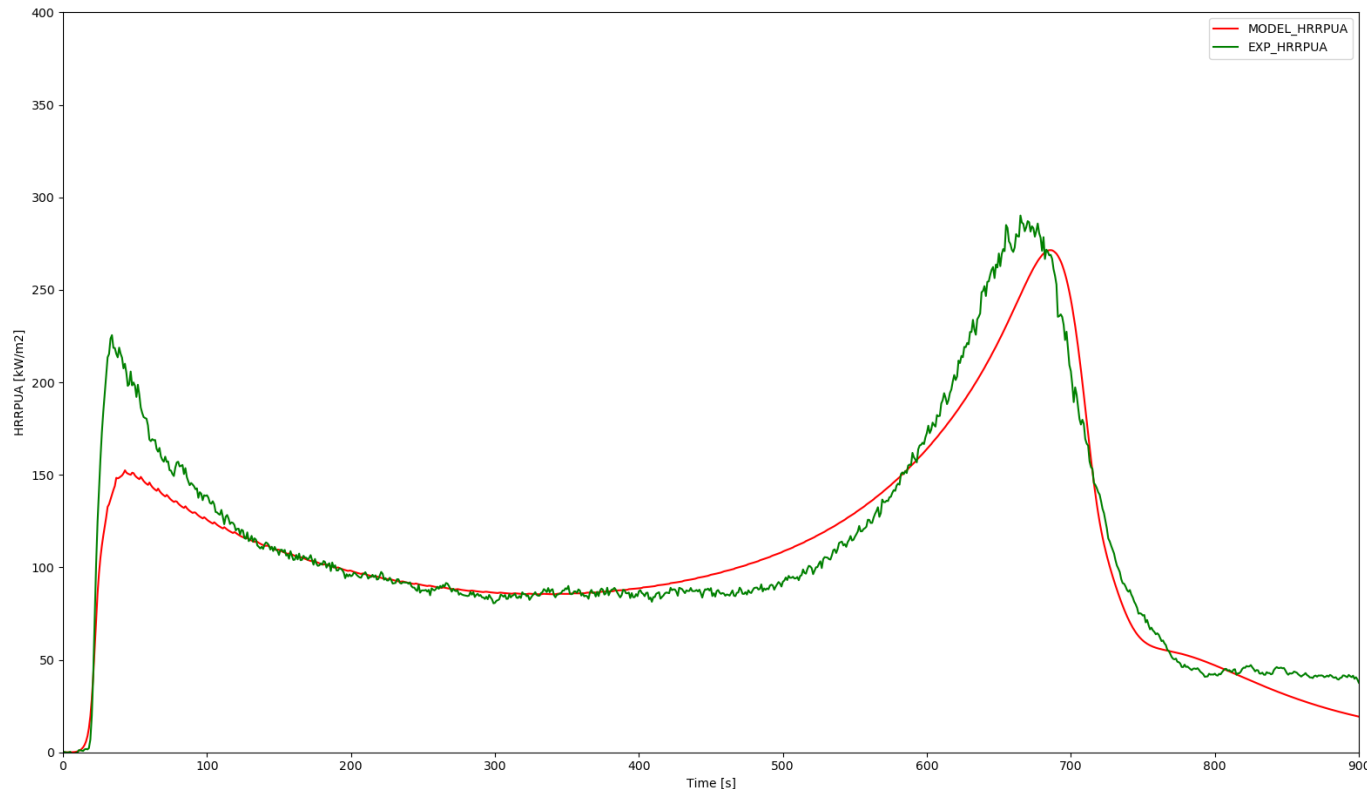
# FDS - PROPTI cone calorimetry model

- Optimized parameters (from 50 kW)
  - $c_s$  of char **0.204** (literature 0.8)
  - $k_s$  of char **0.104** (literature 0.1)
  - $c_s$  of all 3 wood components **2.509** (literature 1.221)
  - $k_s$  of all 3 wood components **0.177** (literature 0.098)



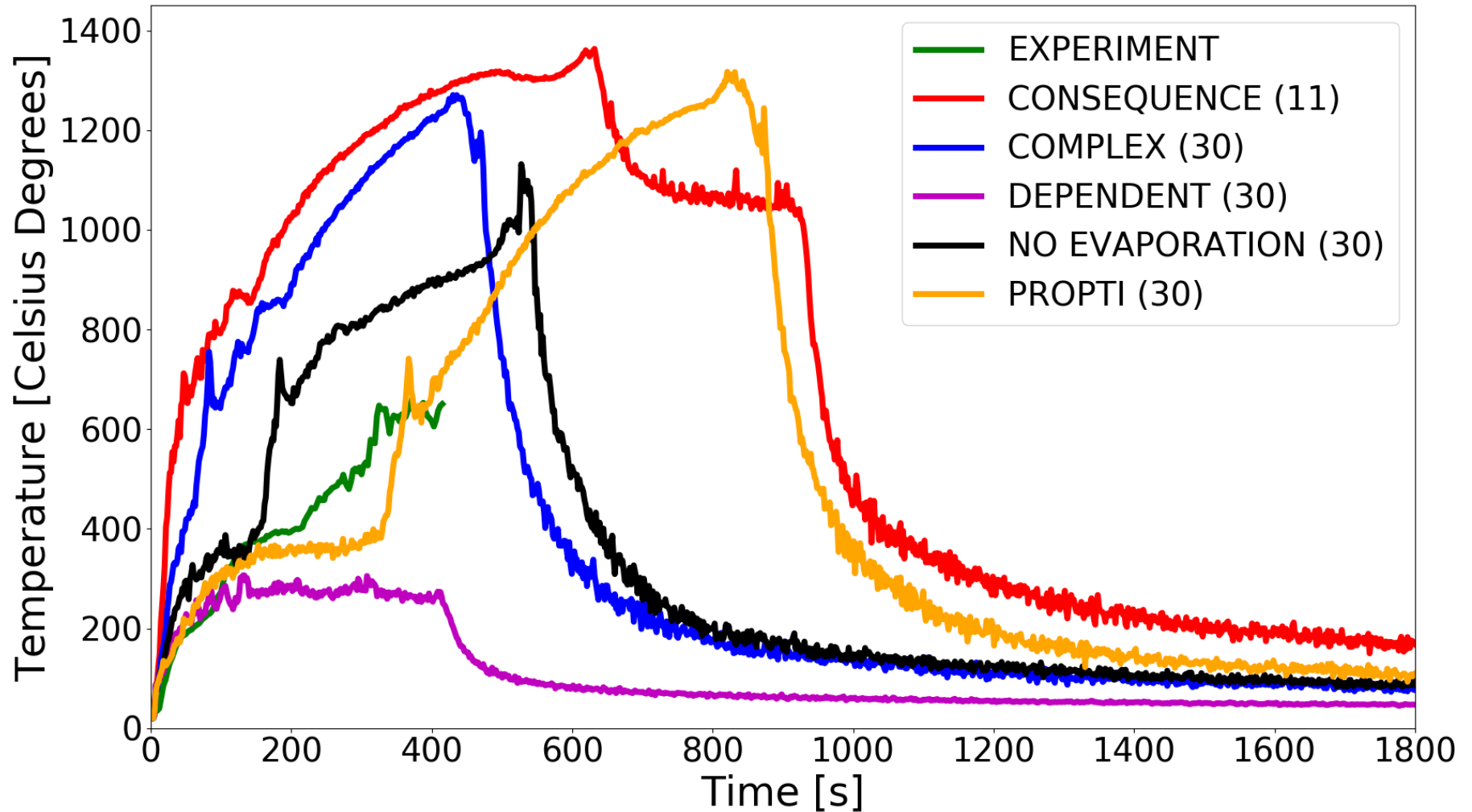
# FDS - PROPTI cone calorimetry model

- $c_s$  of char **0.222** (literature 0.8)
- $k_s$  of char **0.083** (literature 0.1)
- $c_s$  of all 3 wood components **2.356** (literature 1.221)
- $k_s$  of all 3 wood components **0.179** (literature 0.098)
- $\Delta H_C$  of all 3 wood components **15756** (experiment 11710)

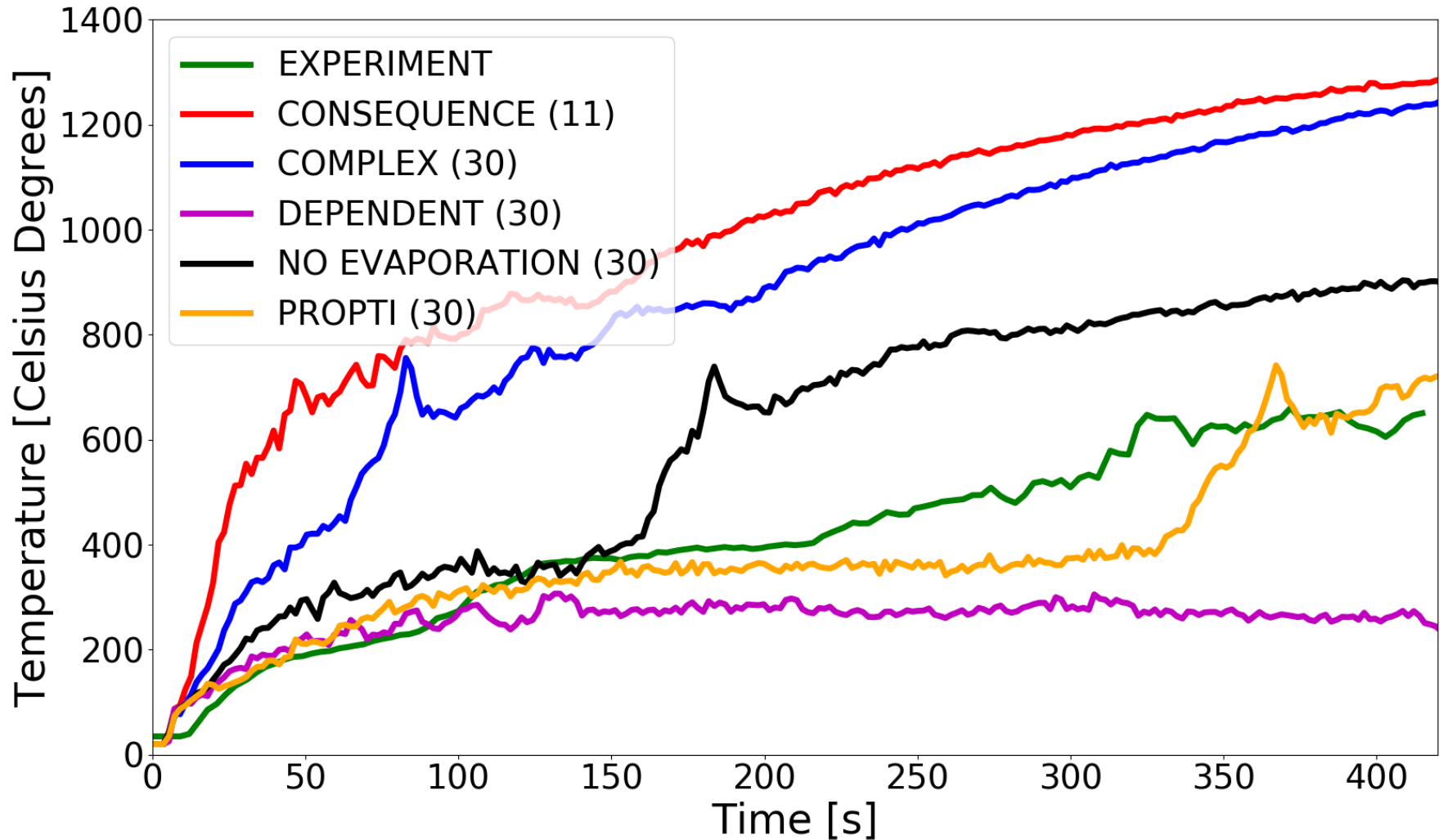




# Experimental Data - Comparison



# Experimental Data - Comparison



# Conclusions and Future Work

- Solid phase discretization
- Promising RCT model outputs using PROPTI
- Thermal properties from cone at different heat flows (PROPTI)
- Different materials (spruce, chipboard)
- More detailed cone model using HT3D and char properties

# Thank you for your attention

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